



# Development of Direct Ammonia Fuel Cells for Efficient Stationary CHP Applications Andrew McFarlan

CLEAN ENERGY TECHNOLOGIES

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# Rationale for Direct Ammonia Fuel Cells







#### **Current alternatives for hydrogen supply**

#### Large scale hydrogen production



To fuelling stations with tube truck as either CH2 or LH2



To fuelling stations with pipelines from central production unit

#### Local hydrogen production



On-site water electrolysis on fuelling station based on electricity and water



On-site natural gas reforming on fuelling station

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Other alternatives:

H<sub>2</sub> from ammonia

H<sub>2</sub> from methanol

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Source: Norsk Hydro



# Large scale CO<sub>2</sub> free hydrogen production



#### Source: Norsk Hydro





#### **Overall Efficiency and CO<sub>2</sub> Emissions During Production and Distribution of Hydrogen Energy Carriers**

(H. Anderson, World Hydrogen Energy Conference, Montreal, 2002)

Conclusions drawn from studies done by Norsk Hydro:

- CO<sub>2</sub> capture and sequestration contributes only slightly to the losses in the full hydrogen value chain
- Central hydrogen and ammonia production seem to be the most efficient way to produce CO2-free energy carriers
- Ammonia infrastructure development is easier because truck transport is possible – supply and demand will be in balance through time
- On site natural gas reforming and methanol steam reforming have highest CO<sub>2</sub> emissions





#### How does ammonia measure up as a fuel for fuel cells?

Fuel property	Ammonia	Methanol
Energy consumed to make, GJ/m.t	t. 27-28	28-31
Energy density, MJ/Kg (HHV)	22.5	22.7
Hydrogen content, % by weight	17.8	12.6
CO <sub>2</sub> emissions, Kg/Kg	0	1.38
Hazards	nonflammable toxic	flammable toxic
Transport/Storage	corrosive liquified gas 126 psia@20°C	noncorrosive liquid
Volume equiv. to 50L gasoline	137	101



# Solid Electrolyte Ammonia Fuel Cell

## What is the concept?

- Ammonia is catalytically decomposed to N<sub>2</sub> + H<sub>2</sub> at anode
- high temperature, low pressure favors
  equilibrium limited decomposition
- Protons transport across a solid proton conducting electrolyte.
- Removal of hydrogen at the anode drives decomposition reaction to completion.
- H<sub>2</sub>/air oxidation at the cathode provides chemical driving force for the fuel cell AND provides the heat of reaction for ammonia decomposition.
- Products of the fuel cell are nitrogen, water, electric power and heat.





#### Electrochemical Reactions in a Direct Ammonia Fuel Cell Using Proton Conducting Electrolyte

**ANODE** (fuel side)

2  $NH_3$  + heat  $\rightarrow$  3  $H_2$  +  $N_2$ 3  $H_2 \rightarrow$  6  $H^+$  + 6 e<sup>-</sup>

**CATHODE** (air side)

 $3/2 O_2 + 6 e^- \rightarrow 3 O^{2-}$  $6 H^+ + 3 O^{2-} \rightarrow 3 H_2O + heat$ 

# OVERALL $2 \operatorname{NH}_3 + 3/2 \operatorname{O}_2 \rightarrow \operatorname{N}_2 + 3 \operatorname{H}_2\operatorname{O}_2$







Ammonia Cracking

$$2 \text{ NH}_3 \longrightarrow \text{N}_2 + 3 \text{ H}_2$$

 $\Delta H = 92.4 \text{ kJ/mol}$  $= 2.7 \text{ MJ/kg NH}_3$ 



9.0 MJ/kg-h 2.5 kW thermal

10.8 MJ/kg-h 3.0 kWe ~55% eff.

-22.5MJ/kg-h

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**Relative Cost of Ammonia as Fuel for "Green" Electricity** 

The historical market price of anhydrous ammonia in the past decade has been about \$150/ton:

At \$150/ton, the fuel cost of electricity is:\$0.05/KWHAt \$300/ton...\$0.10/KWH

In Q4 2003, Ontario wholesale spot market for electricity (NGCC power at \$7MMBtu/MWH) was around \$0.05/KWH. Renewable "Green" power traded at around \$0.09-\$0.10/KWH.

A CO<sub>2</sub> emissions penalty of \$150/ton for electricity generation is equivalent to about 0.05/KWH (NGCC).







# Fuel Cell Materials R&D Activities





#### **Doubly-doped BCGP electrolyte**



Powder XRD patterns of BaCe<sub>0.8</sub>Gd<sub>0.2-X</sub>Pr<sub>X</sub> where X=0.1(a), X=0.05 (b), X=0.02 (c), X=0.015 (d), X=0.01 (e), X=0.005 (f).



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# Pt/BCGP/Pt Ammonia Single Cell Fuel Cell

- Cell performance as a function of Pr concentration (700°C).
- Optimization at approximately Pr – 0.05 (BaCe<sub>0.8</sub>Gd<sub>0.15</sub>Pr<sub>0.05</sub>).
- Related to increased material density and decrease of cell unit volume



Fuel Cells, volume 7, issue 4 (2007) 323.

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# Pt/BCGP/Pt Ammonia Single Cell Fuel Cell



Fuel Cells, volume 7, issue 4 (2007) 323.

 Cell performance as a function of temperature with BaCe<sub>0.8</sub>Gd<sub>0.15</sub>Pr<sub>0.05</sub> electrolyte.

- Difference between hydrogen and ammonia is greater at lower temperatures.
- As the temperature is lowered, the amount of unconverted ammonia in the anode gas stream increases.
- Ammonia FC will require an efficient ammonia cracking catalyst to replace the costly Pt.





## Mixed ionic and electronic conducting anode

- Europium-doped barium cerate material (BCE) proved to be a mixed conducting electrolyte (high ionic and electronic conduction).
- NiO/BCE cermet is a better ammonia cracking catalyst than Pt. Even compositions with NiO concentrations as low as 1%.
- In a monolithic electrolyte supported FC, ammonia cracks at a lower temperature with the NiO/BCE anode than with a Pt anode.
- NiO/BCE is an ideal candidate for an anode supported material.



J. Power Sources 2007, (in press)





## Mixed ionic and electronic conducting anode





#### Anode supported cell development



SEM micrograph (back-scatter mode) of sintered BCGP electrolyte surface coated on NiO-BCE anode.



# Cross-section SEM of NiO-BCE anode supported BCGP with Pt cathode.





#### Anode supported cell development

- Co-pressed application of yttriadoped barium cerate (BCY) on anode support, yielded a 50 µm thick electrolyte (a).
- Thinner layers (10-15 µm) of BCY were deposited by wet colloidal spray combined with a cold isostatic pressing (CIP) treatment (b).
- Composite cathodes (BSCF and BCZY) demonstrated high performance providing alternatives for the costly Pt (c).



*I-V* characteristics of anode supported cells at  $600^{\circ}$ C under fuel mixture of 75% H<sub>2</sub> and 25% N<sub>2</sub>.







# R&D Activities Using Commercially Available Conventional SOFC







Agreement from industry partners (fuel cell manufacturer, ammonia producer) to modify a natural gas fueled 5KW SOFC system to run on anhydrous ammonia, and to conduct a field trial at a suitable site.





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#### **Commercial Opportunities for Direct Ammonia Fuel Cells**

- In late 2006 Acumentrics Ltd. acquired assets and key personnel from Fuel Cell Technologies Inc. and established a Canadian subsidiary in Kingston Ont.
- FCT's core expert team, as Acumentrics Canada, will continue to develop and commercialize SOFC systems using the US-based parent company's proprietary SOFC technology.
- A contract is being finalized which will allow Acumentrics Canada to begin work on testing ammonia in their proprietary SOFC stack.









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# **Thank You**



