

Combustion of Ammonia for Reduced CO₂ in Heating and Power Generation Systems

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Outline

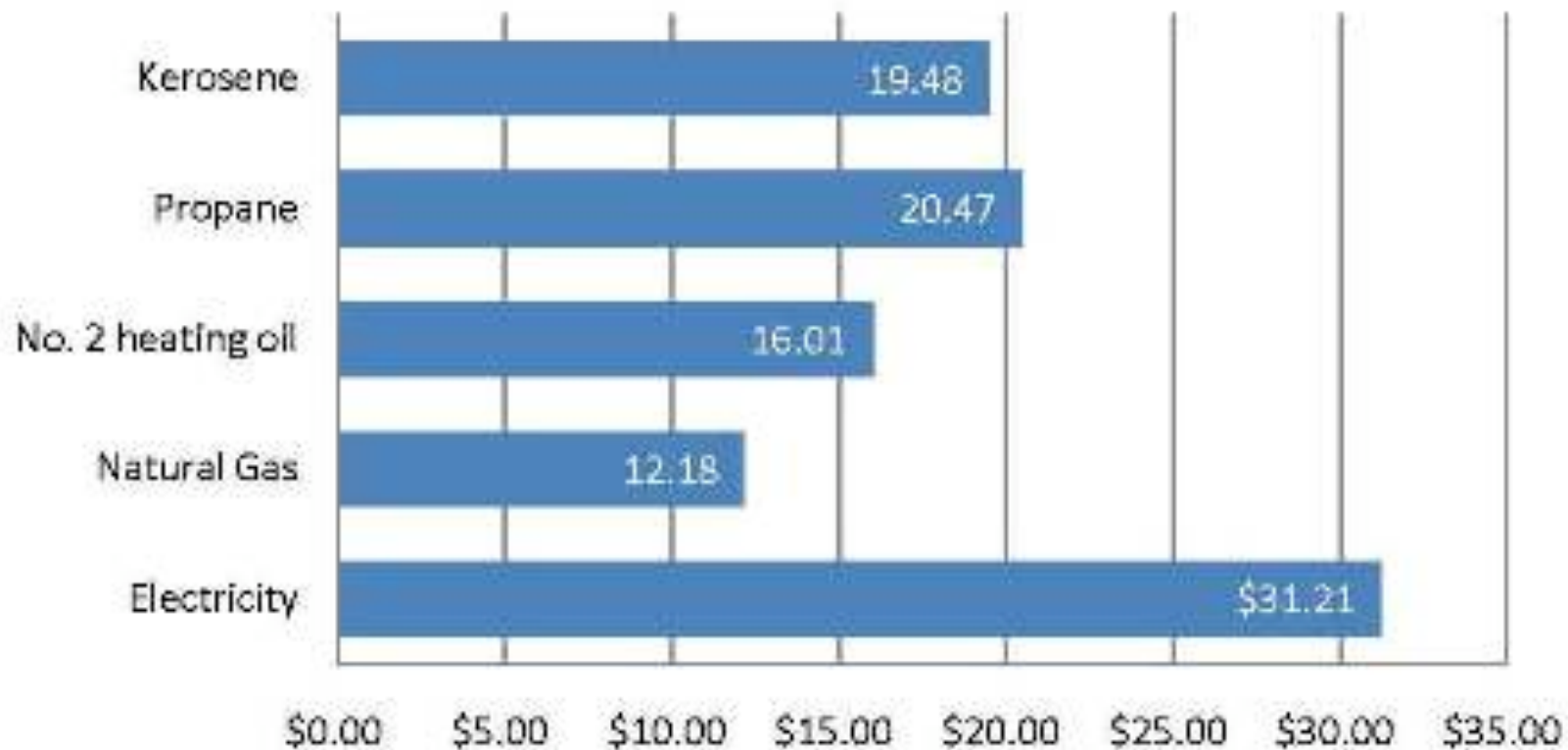


- Motivation
- Background
- Laminar Flame
- Swirl-Stabilized Flame
- Conclusions
- Future Work
- Acknowledgments

Motivation



- 60% of homes in Northeast U.S. heated by heating oil
- Residential cost/MMBtu (DOE 2007)



Background



- Reiter et al., Energy & Fuels, 2008, 95% replacement in IC engines
- Ciccarelli et al., Combust. Flame, 2006 – Flammability limits of $\text{NH}_3\text{-H}_2\text{-N}_2$ -air mixtures widen from 400 C to 600 C
- Brandhorst et al., AIAA 2008-5610 – Ammonia combustion with Ni catalyst
- Less work has been done focusing on furnaces

Initial Tests in Laminar Flame

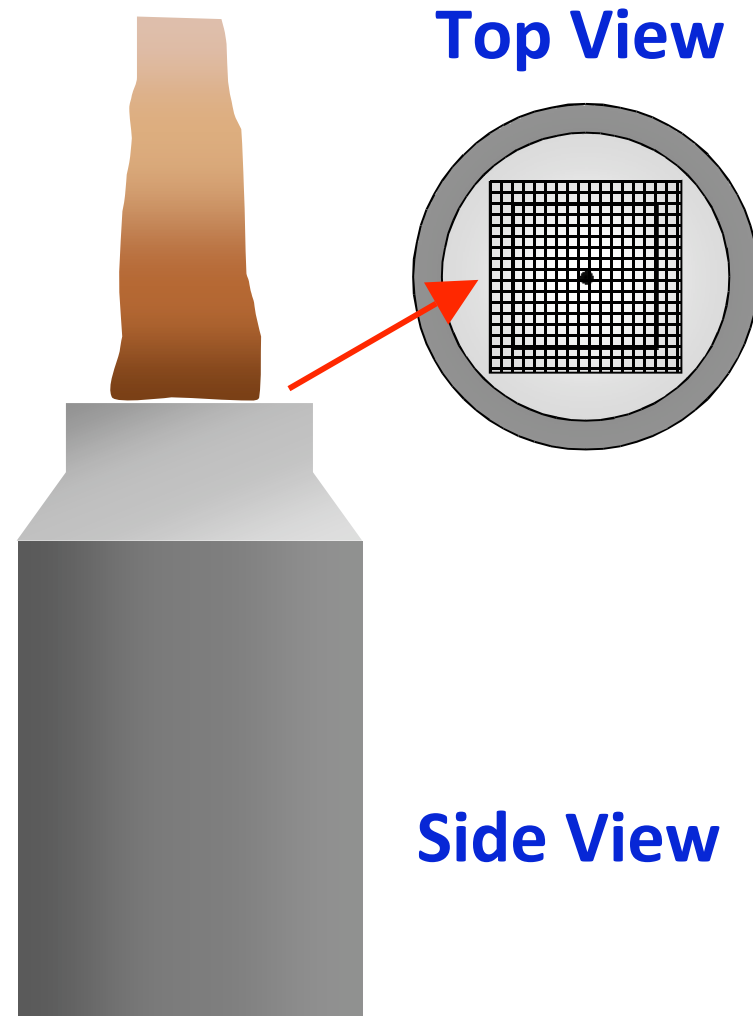
Laminar Diffusion Flame (Hencken Burner)

Fuels

- Ammonia
- Natural gas
- Hydrogen

Oxidizer

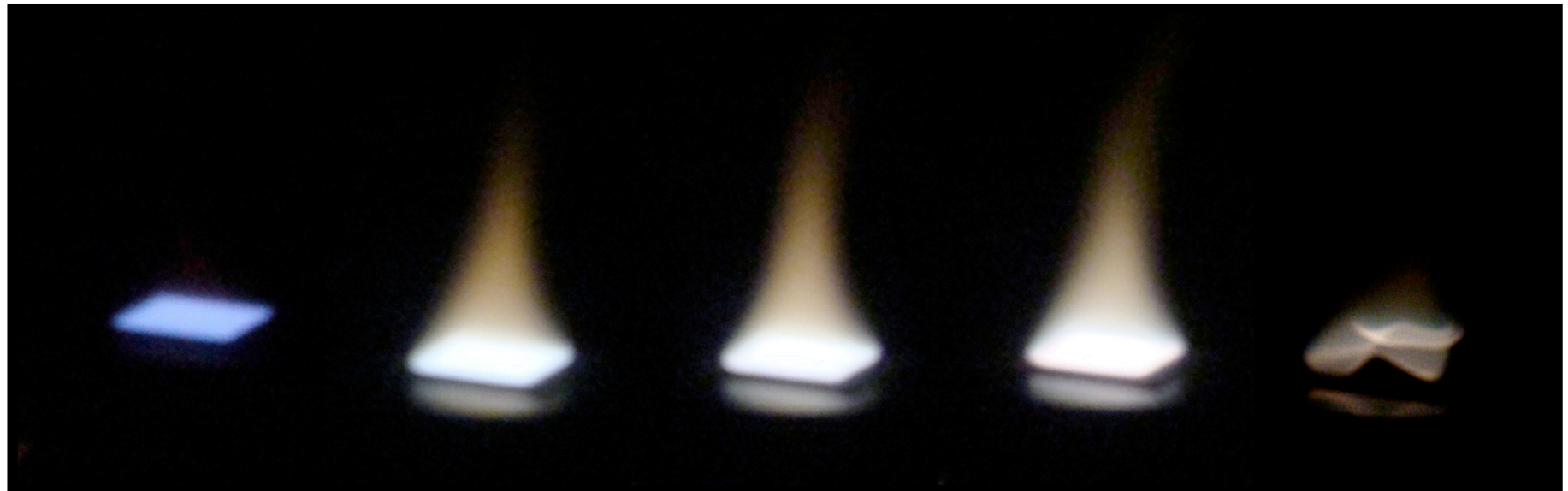
- Air



Results – Laminar Flame with CH₄



NH₃ % Energy in CH₄ @ Equiv. Ratio = 0.95



0%

11%

23%

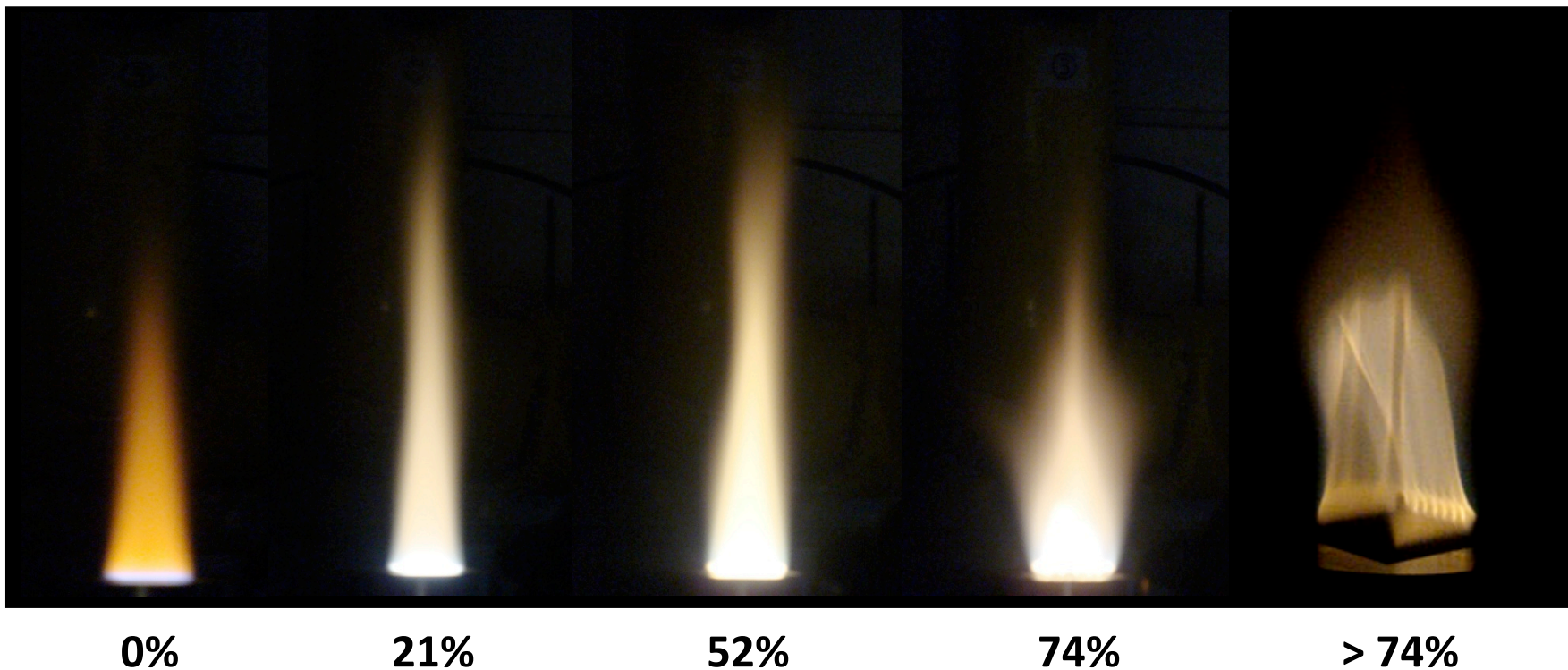
35%

47%

Results – Laminar Flame with H₂



NH₃ % Energy in CH₄ @ Equiv. Ratio = 0.95



Experimental Set-Up – Swirl Flame

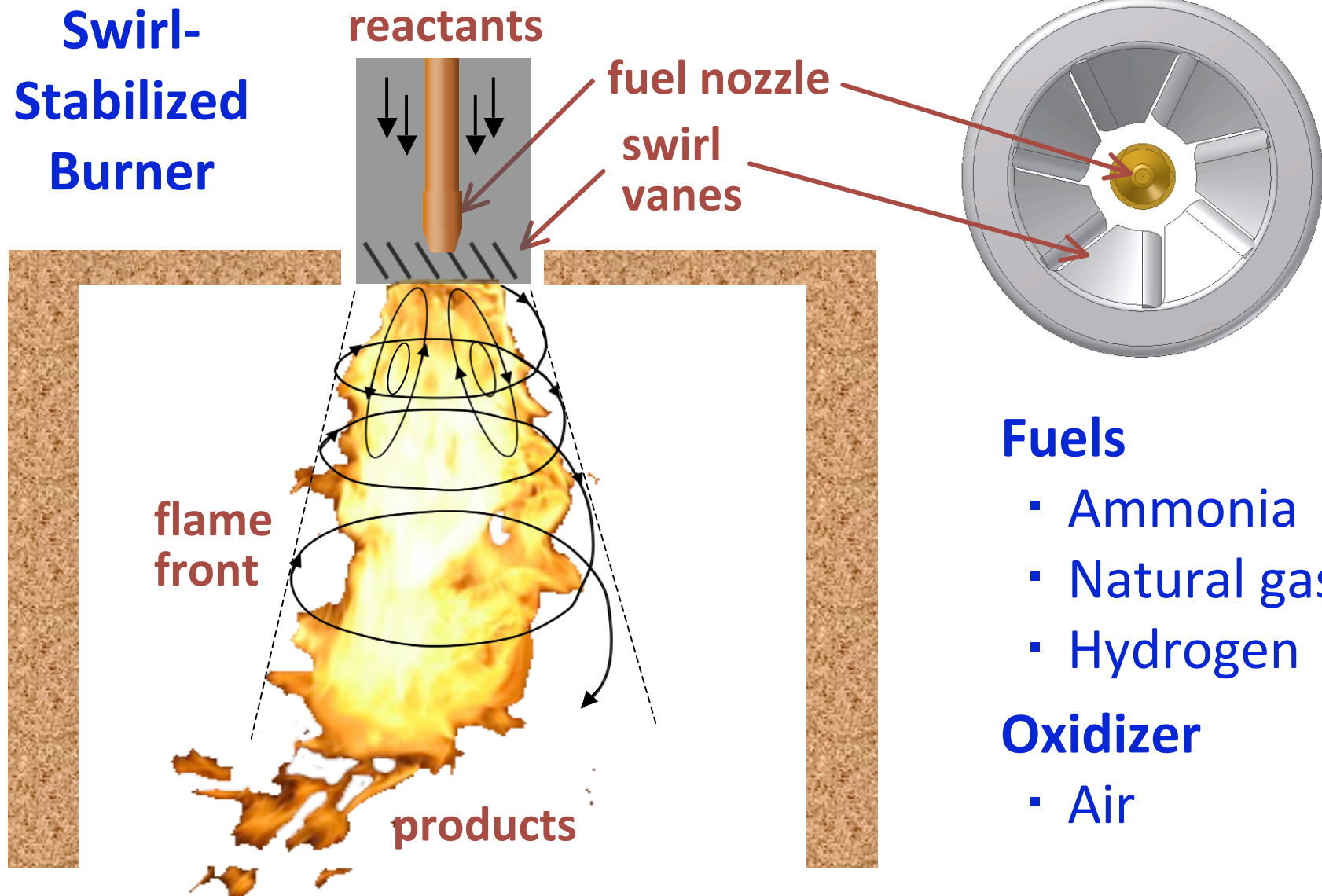


Modified domestic fuel oil burner (< 40 kW)

- Chamber size
- Fuel atomization
- Thermal management
- Custom air swirler
- Optical access
- Temperature and Pressure measurements
- NO_x measured in exhaust



Experimental Set-Up



Flame Comparisons

**Fuel Oil
(28 kW)**



**60% NH₃ by Energy
in H₂ (15 KW)**



**34% NH₃ by Energy
in CH₄ (5 kW)**

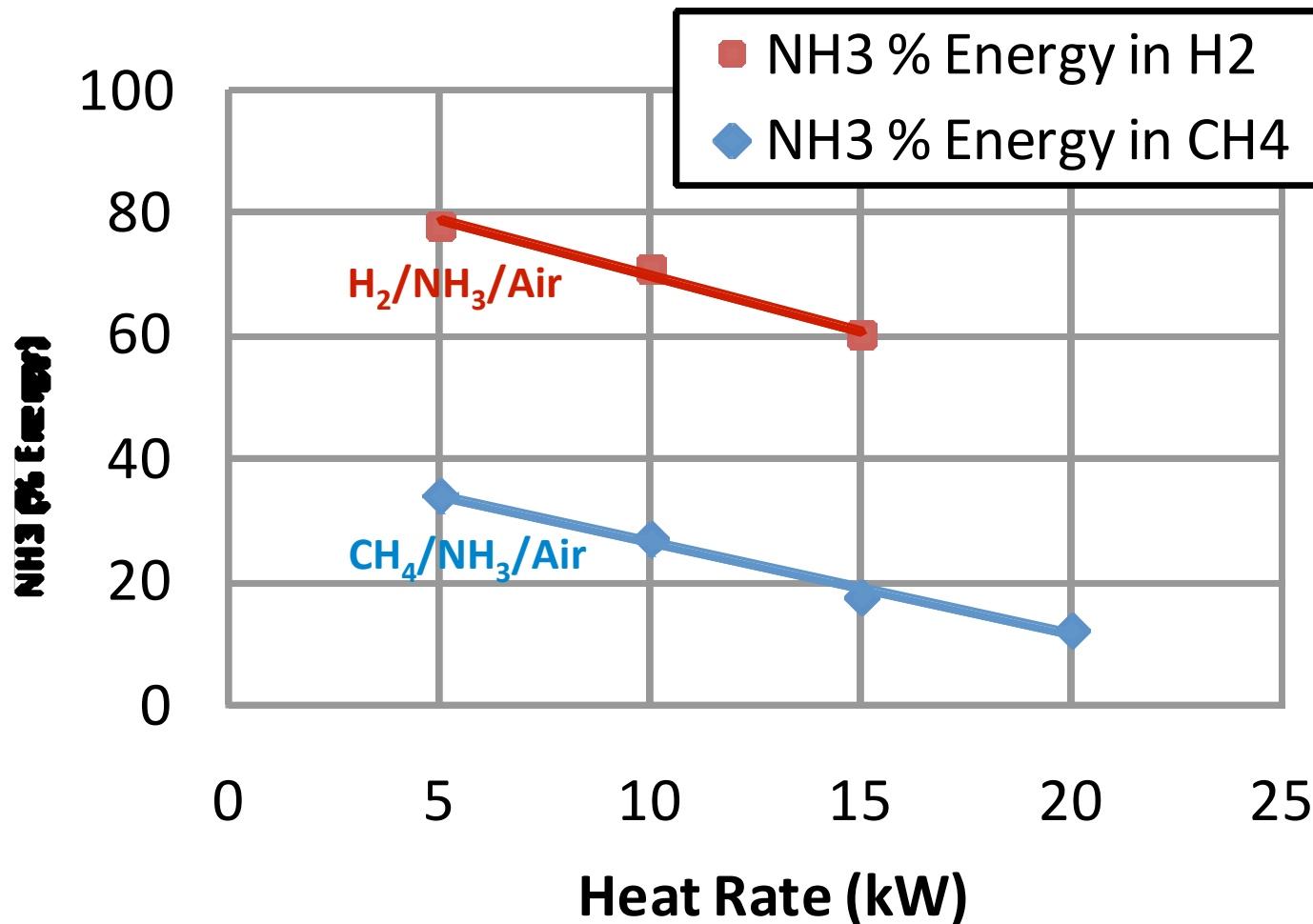


Study of Natural Gas (CH_4) and Hydrogen (H_2) Replacement

- Effect of heat rate on NH_3 % by energy
- Effect of air preheat on NH_3 % by energy

Results – Effect of Heat Rate

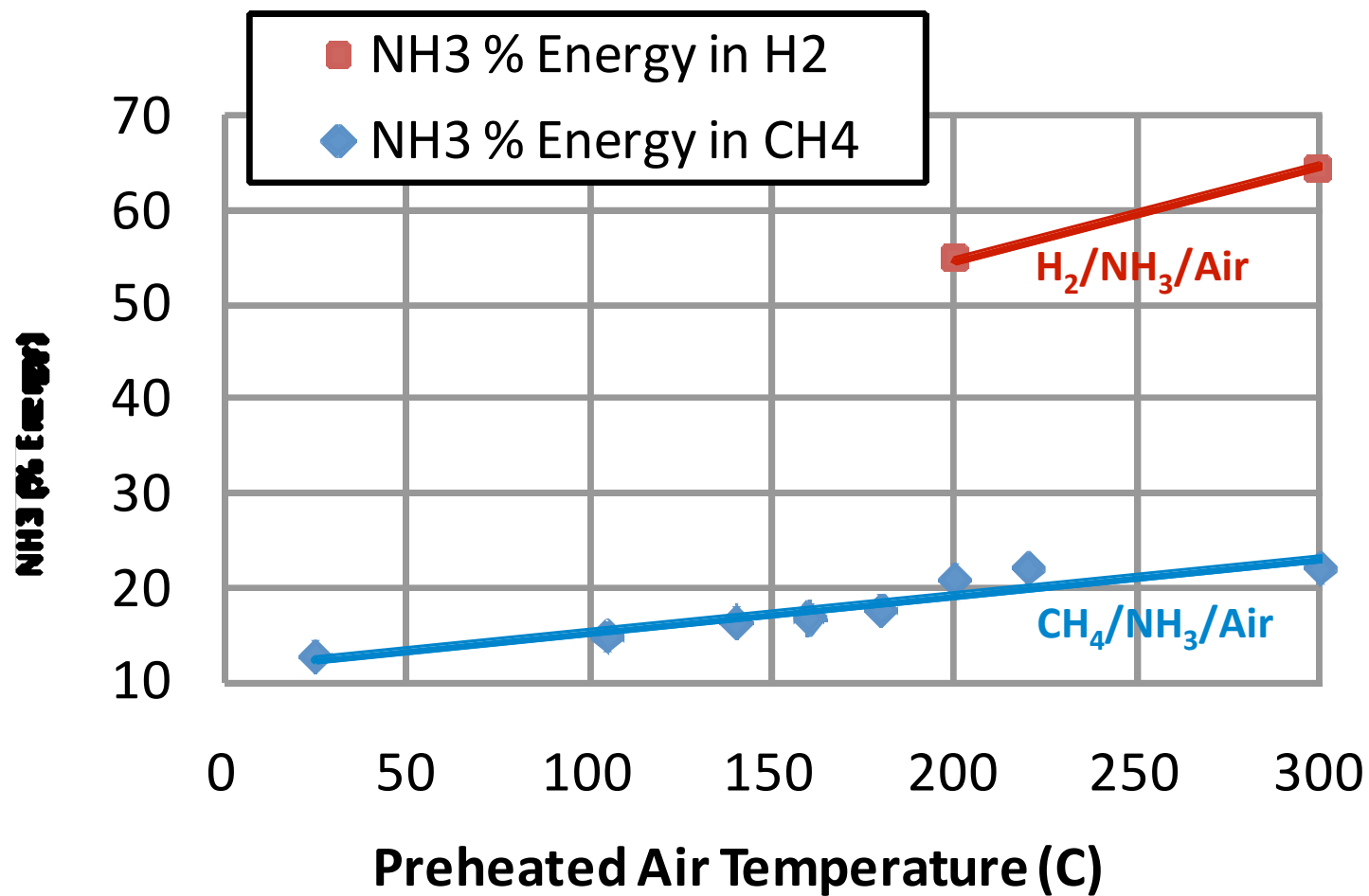
CH₄/NH₃/Air & H₂/NH₃/Air (Equiv. Ratio = 1.0)



Results – Effect of Air Preheat



CH₄/NH₃/Air & H₂/NH₃/Air @ 15 kW (Equiv. Ratio = 1.0)

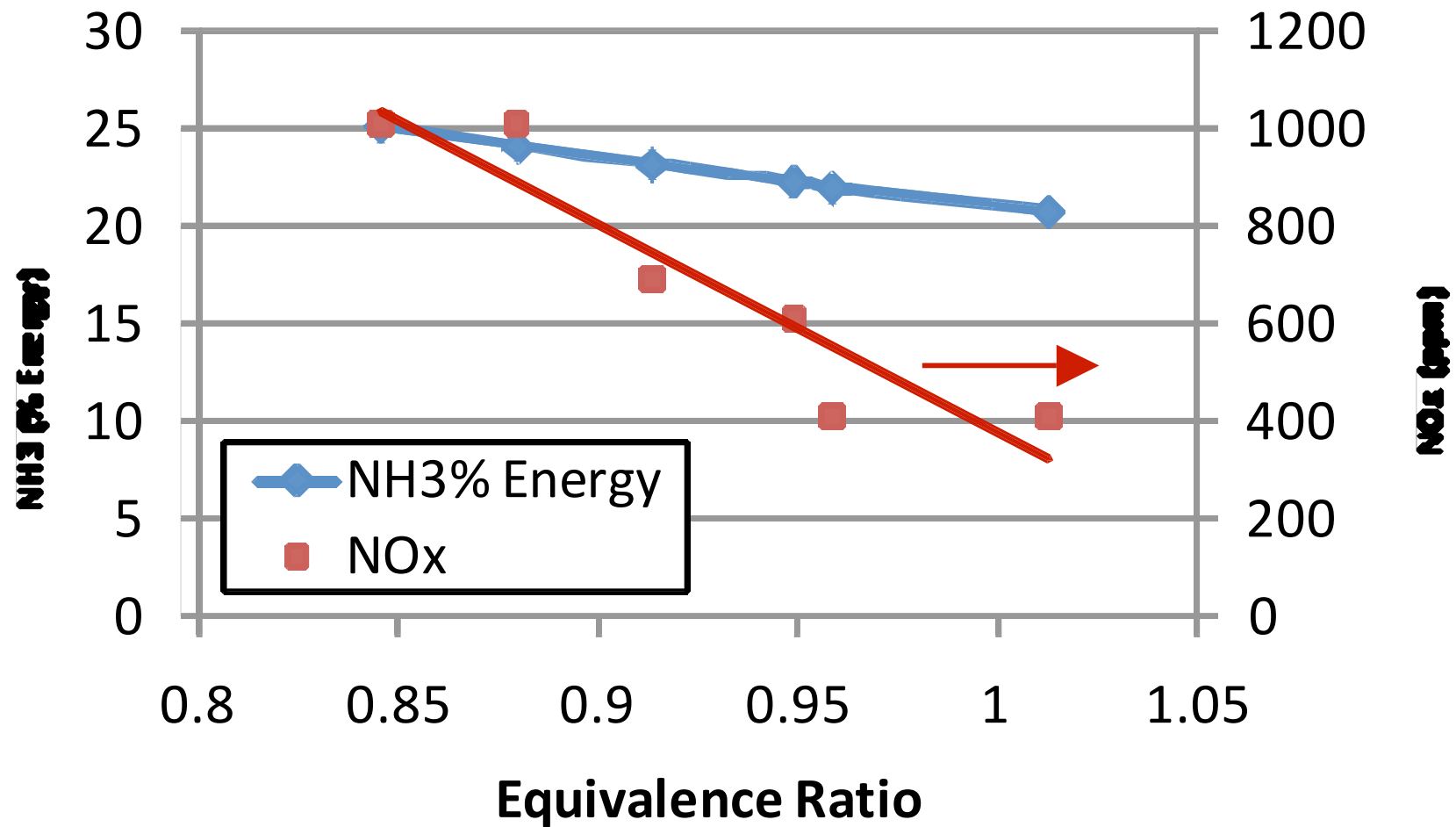


Study of Natural Gas (CH₄) Replacement

- Effect of equivalence ratio on NH₃ % by energy and NO_x**
- Effect of nozzle position on NH₃ % by energy and NO_x**

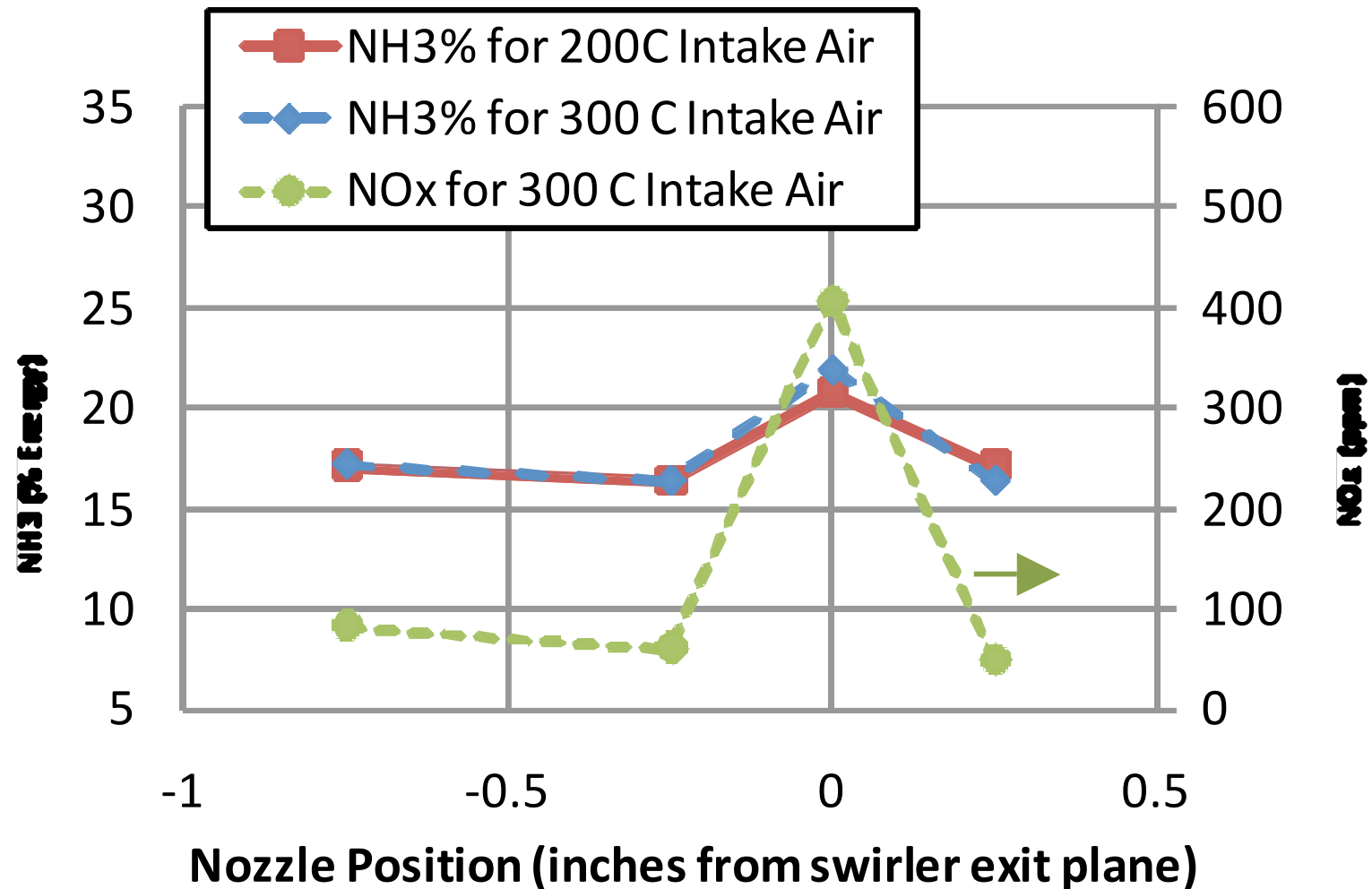
Results – Effect of Equiv. Ratio

CH₄/NH₃/Air @ 15 kW (300 C Intake Air)



Results – Effect of Nozzle Position

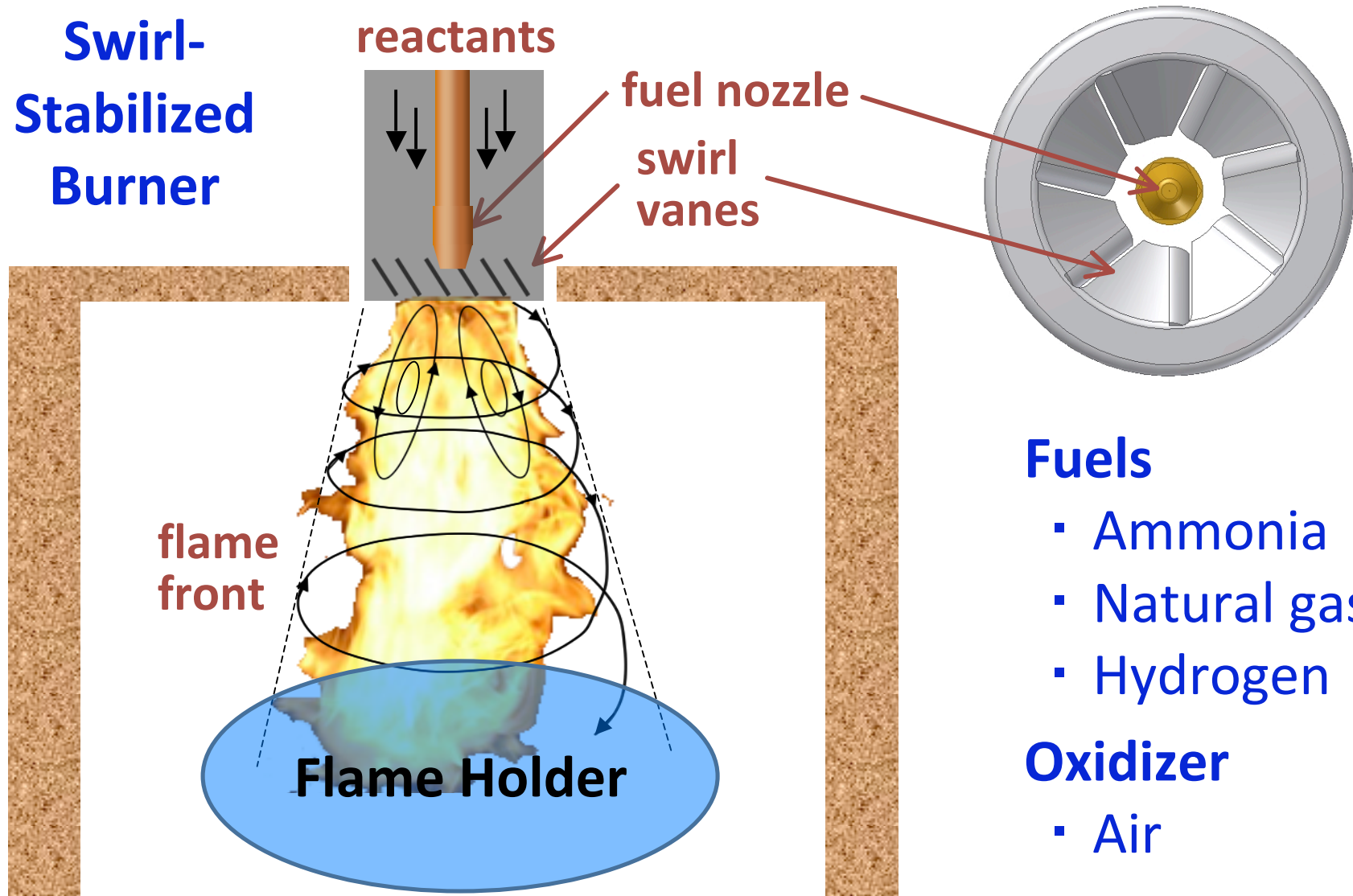
CH₄/NH₃/Air @ 15 kW (Equiv. Ratio = 1.0)



Study of Natural Gas (CH_4) and Hydrogen (H_2) Replacement

- Effect of flame holder on NH_3 % Energy and NO_x**

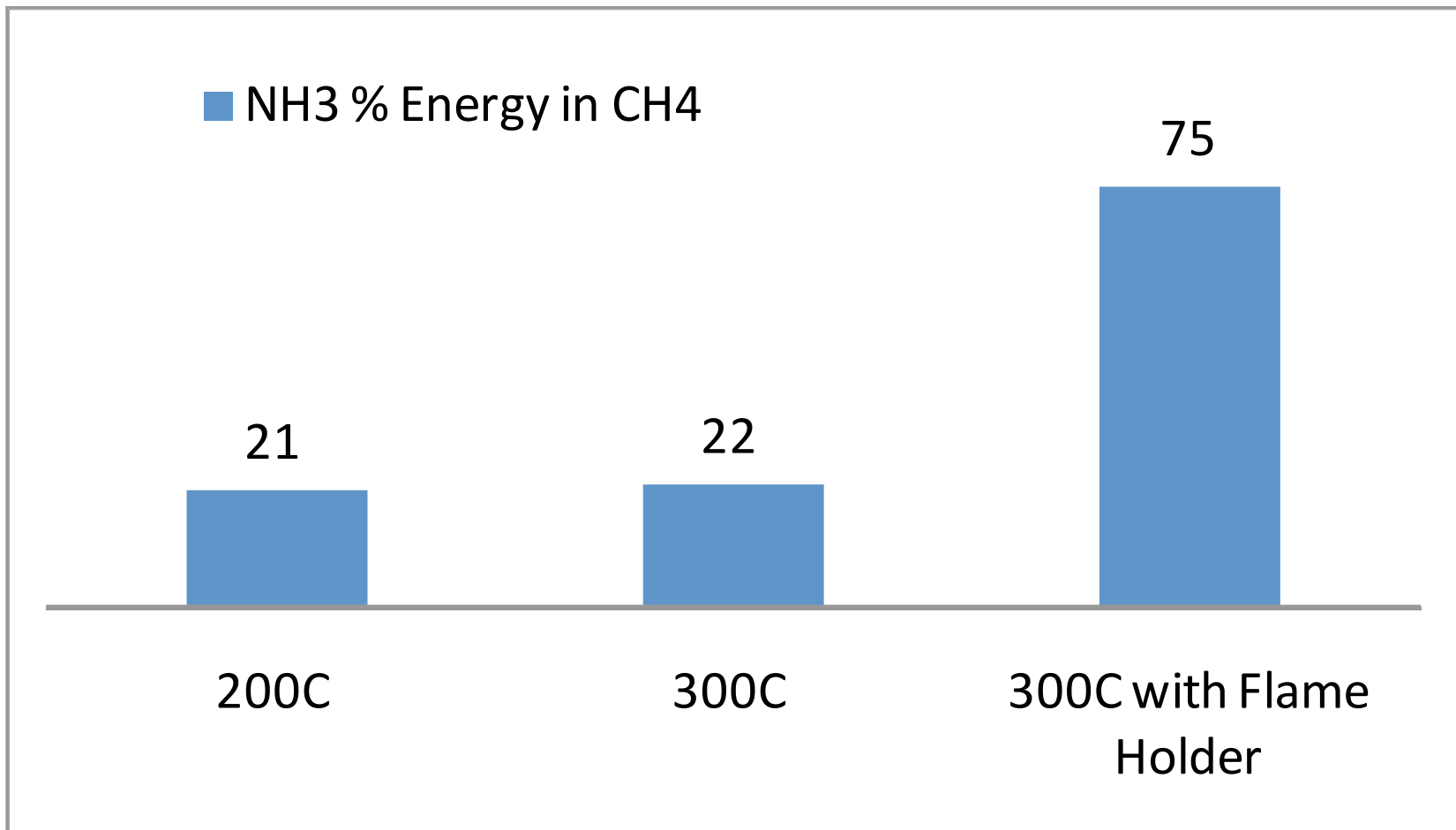
Experimental Set-Up



Results – Effect of Flame Holder



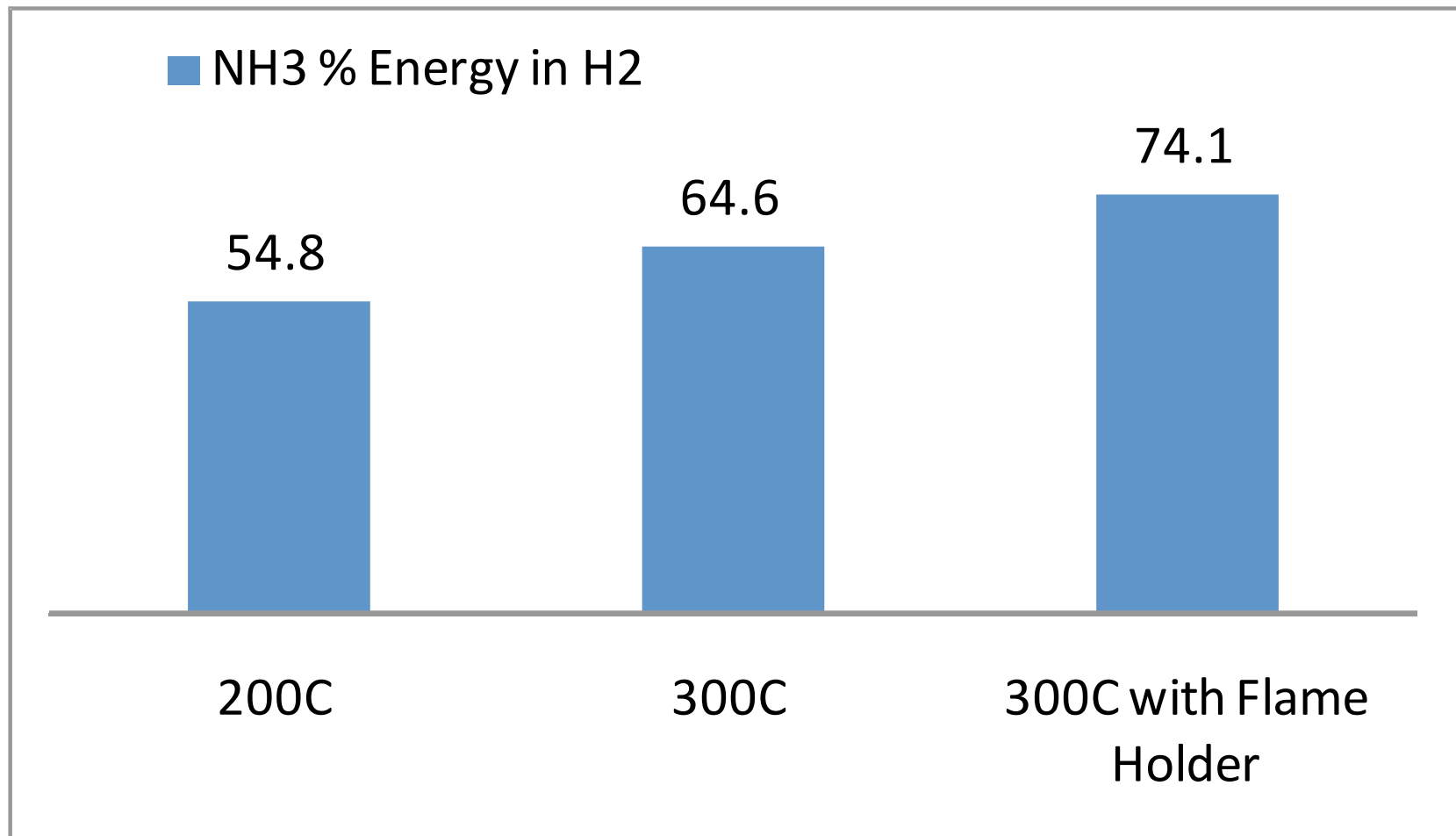
CH₄/NH₃/Air @ 12 kW (Equiv. Ratio = 1)



Results – Effect of Flame Holder



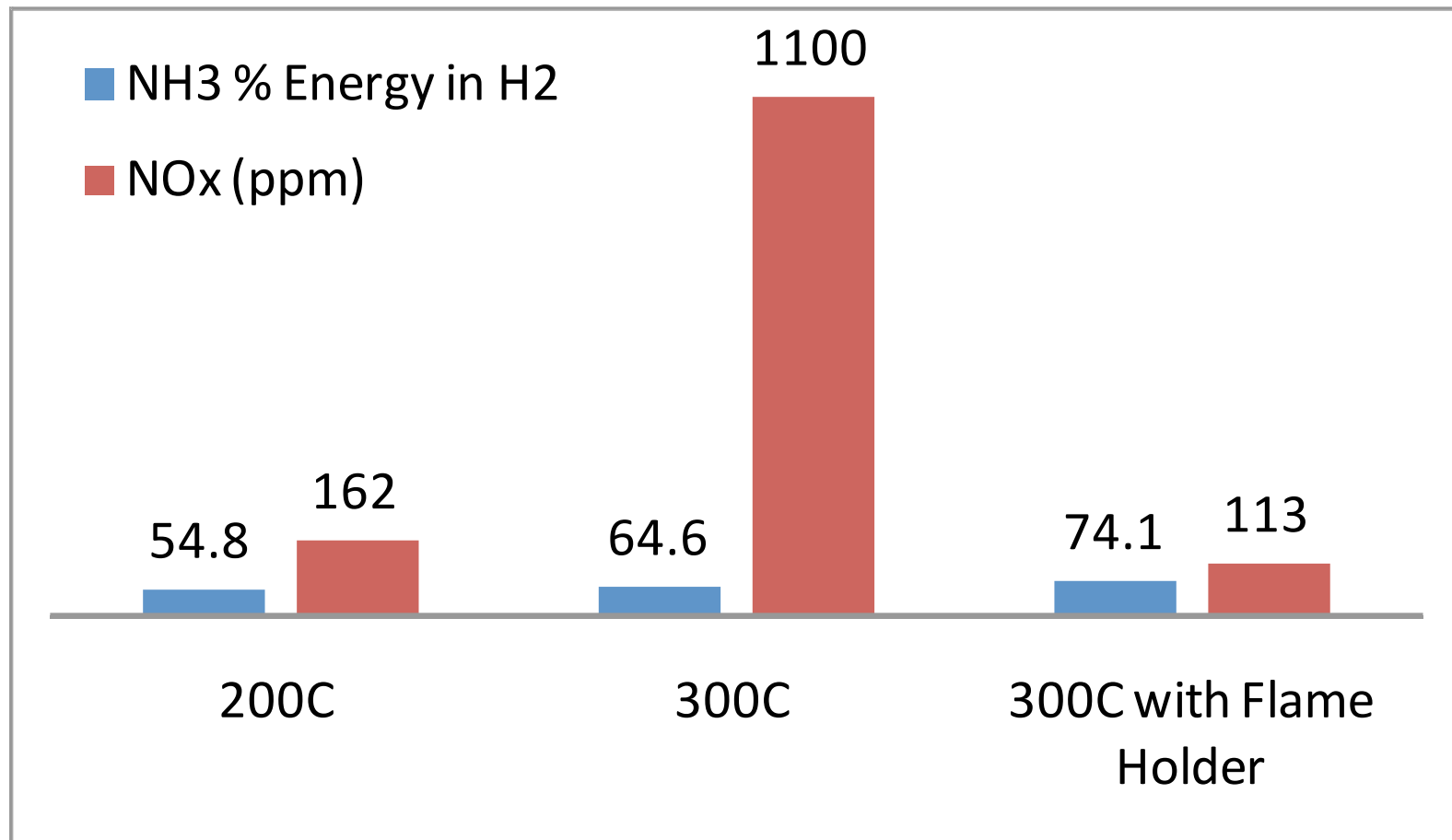
CH₄/H₂/Air @ 15 kW (Equiv. Ratio = 1)



Results – Effect of Flame Holder



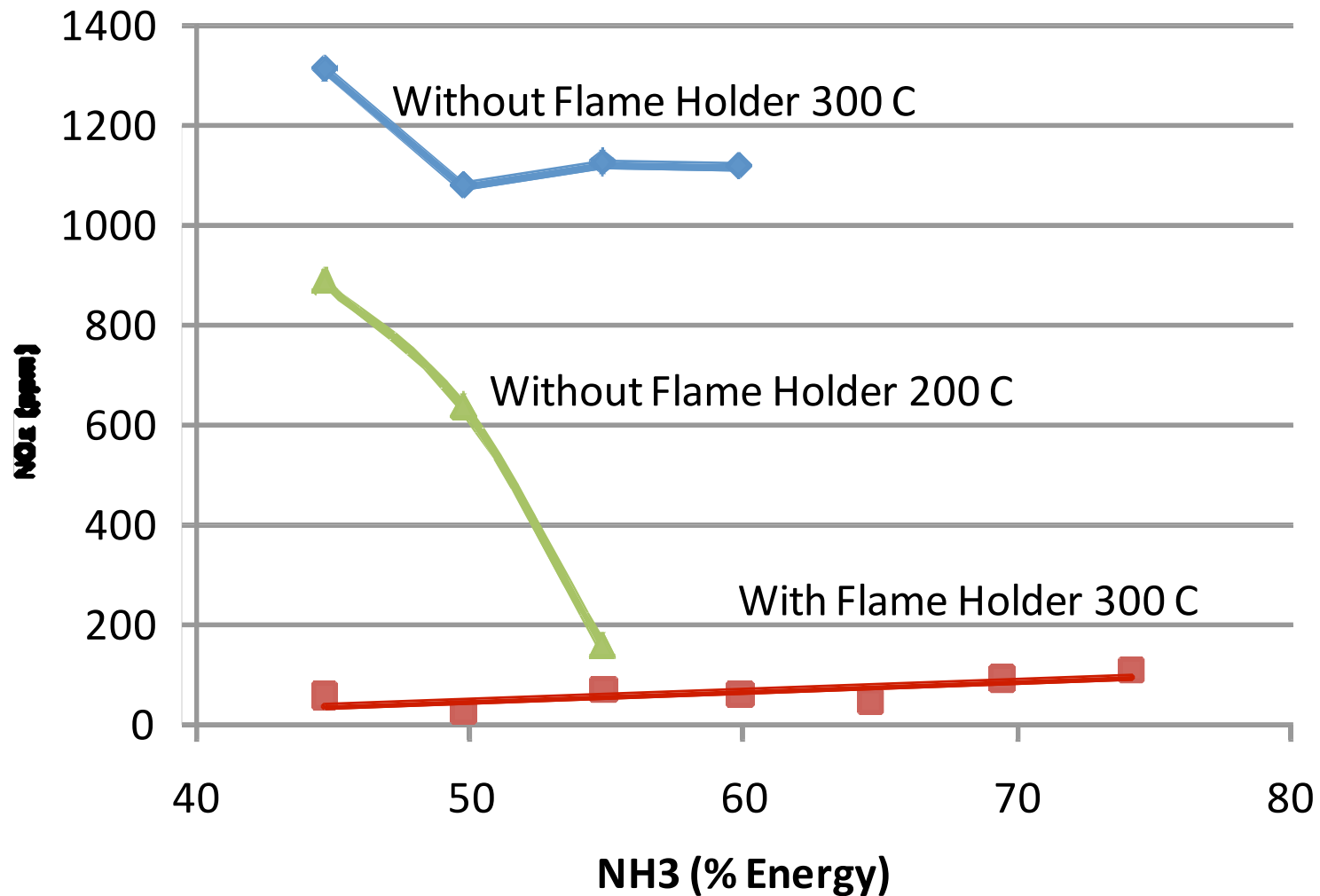
CH₄/H₂/Air @ 15 kW (Equiv. Ratio = 1)



Results – Effect of Flame Holder



CH₄/H₂/Air @ 15 kW (Equiv. Ratio = 1)



Conclusions



- CH₄ replacement
 - NH₃ is tougher at higher heat rates. 20 kW feasible.
 - NH₃ replacement improves with air preheat
 - NH₃ better at fuel lean conditions, but NO_x worse
 - Nozzle position critical effect on NO_x
- H₂ Addition
 - Air preheat has moderate effect, NO_x much worse
 - More NH₃ reduces NO_x with lower preheat (200 C)
- Flame holder improves NH₃ and reduces NO_x

Future Work



- Refine design of chamber
 - Refine design of flame holder
 - Consider use of catalyst
 - In-depth emissions characterization
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- Combustion in furnace designed for natural gas
 - Combustion in turbine combustor

Acknowledgments



- Norm Olson, Iowa Energy Center
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