

Ammonia Neighborhood Energy Stations Opportunities, Markets, Issues

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Assumptions

- Stationary IC engines running on ammonia, designed and run for zero emissions including low NOX (not requiring NOX control) (prototype – Sturman engine)
 - Installed cost \$700 / kw, up to 1.5 MW
 - 45% power efficiency; +40% useable energy for heat/AC in CCHP
- Ammonia at \$250/tonne, Zero Carbon Ammonia at \$350/tonne
- Rectifier/Inverter Power Electronics Microgrid Controller \$100 /kw
- 24/7, 99% available, ultraclean, high quality power sold at \$150 per mWh
- Onsite, ultraclean heat/MP steam/AC sold as byproduct at \$6/MMBTU



Neighborhood Energy Station

- A typical high volume gasoline station can easily dispense 1.5 MM gallons of multiple grades of gasoline/diesel in a year.
- This case examines a 'neighborhood' ammonia energy station of approximately the same scale that could provide power and heat to the neighborhood (or condo or office building or village or light industrial or retail complex).
- This station would house a diesel genset/CHP unit running on ammonia. The prototype for this is a 1.5 MW generator operating at 45% efficiency, designed for combined heat/power taking efficiency up to 85% for medium pressure steam/space and water heating and adsorptive air conditioning.)
- The general complexity of these stations would be less than a gasoline station (single grade, dispensed almost entirely (hardpiped) to the genset(s) instead of retail interface with hundreds of transactions to untrained public per day).
- A typical tank size for ammonia distributors is 30,000 gallons. Underground, chilled tank for safety, security and ease of temp/pressure maintenance.
- Fuel delivery logistics would be similar (11,500 gal tank trucks (typical size ammonia trucks)).
- Very rough project costs \$1.0 MM for ammonia IC genset(s), \$0.15 MM for microgrid controller, \$0.15 MM for underground tank and land. Roughly \$1.5 \$2 MM.



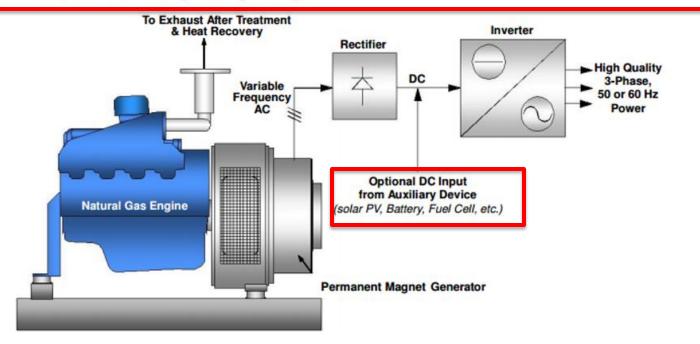
Neighborhood Energy Station Base Operations

- With 3 truck deliveries per week (1.75 MM gal ammonia/year), a 1.5 MW engine can be supplied 85% of the time. The unit would be available 100% of the time (minus maintenance) and could be run at the cost of more frequent ammonia deliveries. At \$250/tonne, 1.75 mm gallons of ammonia costs \$1.0 MM. At \$350/tonne for zero carbon ammonia, the cost is \$1.4 MM
- Running 85% of the time (7450 hrs/yr) produces 11,400 mWh and 35,000 MMBTU of CHP heat (40% of the MMBTU's in the 1.75 mm gal of ammonia)). We will assume conservatively that 17,500 MMBTU of that heat would be effectively used or sold.
- Power revenue 11,400 * \$150 = \$1.7 MM per year
- Heat revenue (at 50% sales) 17,500 * \$6 = \$0.1 MM per year
- Margin \$1.8MM \$1.0 MM = \$0.8 MM
- Margin \$1.8MM \$1.4 MM = \$0.4 MM (for zero carbon power)
- Baseline operation, conservative prices, 85% operation, 50% sales of heat = \$0.4 -\$0.8 per year on \$1.5 - \$2.0 MM investment.



Rectifier/Inverter Power Electronics Microgrid Controller

Because the system can now operate at variable rpm, it maintains a high torque regardless of the output, thus maintaining near full-load efficiency throughout its operating range. Additionally, more output can be derived from the same engine if it can be operated to the higher rpm, that is, beyond the typical synchronous speed of 1800 rpm. Another advantage is that the same machine can be applied to the 50 Hertz market, without de-rating or design changes.



Engine/Generator Output

| RPM | Volts | Freq (hz) | KW |
|------|-------|-----------|-----|
| 1000 | 98 | 135 | 39 |
| 2200 | 207 | 297 | 93 |
| 3000 | 258 | 405 | 130 |

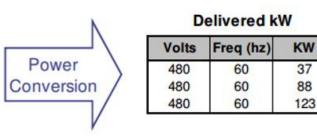


FIGURE 1. CONCEPTUAL DESIGN OF INVERTER-BASED ENGINE GENERATOR



http://bpe-ne.com/wp-content/uploads/2012/07/top10-reasons-to-choose-inverter-based-engine-chp.pdf

Table 2-1. Reciprocating Engine Characteristics

| Size range | Reciprocating engines are available in sizes from 10 kW to over 18 MW. |
|------------------------|---|
| Thermal output | Reciprocating engines can produce hot water, low pressure steam, and chilled water (using an absorption chiller). |
| Fast start-up | The fast start-up capability of reciprocating engines allows timely resumption of the system following a maintenance procedure. In peaking or emergency power applications, reciprocating engines can quickly supply electricity on demand. |
| Black-start capability | In the event of an electric utility outage, reciprocating engines require minimal auxiliary power requirements. Generally only batteries or compressed air are required. |
| Availability | Reciprocating engines have typically demonstrated availability in excess of 95 <i>percent</i> in stationary power generation applications. |
| Part-load operation | The high part-load efficiency of reciprocating engines ensures economical operation in electric load following applications. |
| Reliability and life | Reciprocating engines have proven to be reliable power generators given proper maintenance. |
| Emissions | Diesel engines have relatively high emissions levels of NO_x and particulates. However, natural gas spark ignition engines have improved emissions profiles. |

Reciprocating Engine Characteristics

The following characteristics outline the benefits of medium speed engine technology for ancillary services:

- Operating Flexibility
 - 3 minute starting time
 - Zero startup cost
 - MW/minute ramp rate
 - Regulation (AGC) accuracy
 - Minimum load
 - % load on each engine
 - Multi engine plant
- Cost
 - Relatively low capital cost
 - Excellent efficiency
 - Excellent part load efficiency

- Emissions
 - HFO, DFO, Natural gas, or Dual Fuel operation
 - No water use
 - Reduction through
- SCR/OxyCad's
- Installation speed
- Siting flexibility
 - Transmission constraints
 - Transmission alternative*
- Reactive power
 - Synchronous condenser clutch?
 - Black start

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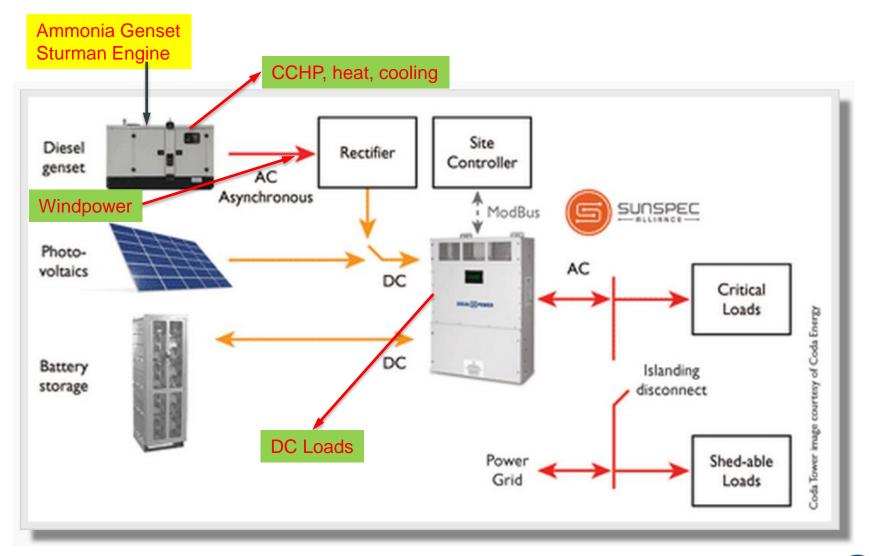
Islanded operation

chp technology doe ic engines.pdf ancillary services presentation caterpillar ic engines.pdf

A Comprehensive Study on Microgrid Technology 2015.pdf



Neighborhood Energy Station – Ideal Power







Neighborhood Energy Station - Microgrid

- Easily accommodate local *variable* renewable solar or wind by cutting back genset (with immediate local load following). Feed DC solar directly prior to inverter. Feed variable frequency wind power into rectifier.
- Pass through solar/wind or ammonia power and ancillary services to the grid. 24/7 availability of peaking power (125% of genset rating typical), frequency regulation, voltage support, black start.
- Provide predictable, centrally addressable reserve available on 5 minute call-up (with right incentives and minimally sophisticated 'smart grid' controls) (much cheaper and much more flexible than spinning reserve CCGT)
- Provide distributed and potentially very substantial regional fuel reserve for midwinter, late summer, regional security (much cheaper (pseudo-'free') than natural gas storage and much more flexible). 30,000 gallon underground tank of ammonia provides about 200 MWh of electricity (45%) and 600 MMBTU of CHP heat (40%), Over 5 days of continuous operation.
- Locally addressable loads via microgrid controller and locally optimized agreements on load priority, demand shedding (e.g., house by house incentives on high thermostat setting when grid power sales are very lucrative).
- Easily integrated systems for local DC loads



Compare to Battery Storage

- 30,000 gal underground tank (similar to gas station) stores about 200 MWh and 600 MMBTU CHP heat.
- About \$100,000 capital cost.
- Cost of Li-ion battery storage \$500 /kWh (2 mWh storage = \$1.0 MM)
- Batteries 10X higher cost for 1% of energy storage (This does not even account for battery replacement every 10 years and no byproduct heat)
- Dispatch available at full power (1.5 MW) for 5.5 days
- Much longer life (genset versus batteries)
- Gensets require more maintenance
- Recharge of 5 days capacity takes about 15 minutes with scheduled deliveries
- Zero carbon 'recharge' from ammonia delivery (does not use local excess power to manage local peaks/valleys). Accesses lowest cost excess power in region.



Compare to Natural Gas Genset

- No need for gas supply
- No new pipelines required (multi hundred million \$ projects, 5 year projects from negotiation thru gas flow, political/public opposition)
- Purchase fuel from multiple sources rather than prices set by pipeline operations
- Reduced exposure to single source price volatility
- Not subject to pipeline/compressor failure (accident, earthquake, terrorism)
- Very low cost local storage of energy (5.5 days of operation without refill) compared to expensive cavern storage backed up by LNG
- No CO2 emissions
- Low/No NOX
- Can be operated in urban or suburban areas
- Access to \$1.50 \$2.00 / MMBTU Stranded Gas for \$250/tonne contracted ammonia



Compare to Transmission/Distribution Infrastructure

- One 80 tonne rail car 225 mWh and 700 mmbtu coproduct heat
- Deliver anywhere in 500 mile radius for \$40/tonne (\$3200/railcar)
- For power 1.5¢ / kWh delivered (with no credit taken for heat)
- No transmission/conversion losses on lines and transformers
- Stored power dispatched as needed
- Flexibility by region/customer, by season, by unanticipated demand
- Responds to regional growth and economic activity
- Inter regional pipelines are much cheaper and safer than gasoline, crude oil or gas pipelines (liquid (pumps, not compressors), less explosive, less environmental risk from spill, no GHG (e.g., CH4), one component (cleaner, more predictable, simpler maintenance))
- Move utility scale power from remote areas with low cost, clean power to large markets (desert solar, Wyoming/Texas wind, Marcellus gas, Alaska gas, Iceland geothermal, Canada hydroelectric)



Neighborhood Energy Station (Upside Revenue Potential)

- Sell 15% of power capacity to high value peaks, 2000 mWh * \$250/mWh = \$0.5 MM
- Island economies that must generate their power from fuel oil (Hawaii, Caribbean, Alaska, Indonesia). Fuel oil is \$30-\$40 per mmbtu.
- Medium scale distribution/retail (frozen/refrigerated foods), light industry and agriculture utilizing refrigeration, medium pressure steam or drying (e.g., crops) that place high value on the associated heat)
- Regions that place high value on pure water (exhaust from ammonia Sturman engine is water and nitrogen. Pure water can be captured at the cost of condensing the water.) Combustion of 1.75 MM gallons of ammonia generates about 1.7 MM gallons of water.
- They will be very attractive to sites willing and able to pay large premiums for locally controlled, uninterruptible power (financial/business centers, server farms, hospitals, military/government installations, large research facilities/research universities)
- Regions that are imposing a cost on CO2 emissions can reduce or eliminate those costs. Clean Power Plan. State Plans.
- Grid ancillary services. Load following, Peak power, Voltage/frequency regulation, Locational value, Black start



For the Future, Basis for Other Systems

- Initial infrastructure for ammonia IC engines for buses, delivery trucks, taxis, government vehicles etc for superclean transport in cities (much cheaper than CNG or electric, or hydrogen).
- Clusters of microgrids in cities for larger scale integration into district heating, cooling, demand management and integration of renewables.
- Consolidate delivery infrastructure for urban clusters. Low cost pipeline networks to deliver ammonia to microgrids throughout a region from central depots. Reduces truck traffic, labor, transfer/collision risk. Improves inventory flexibility and supply chain efficiency.
- Incremental targeted investment in clean energy production that produces its own revenue (unlike large generation plants on spinning reserve, pipelines or HVDC). Very good size for financing by utilities or municipalities (or for partnerships with coops or third party turnkey or service providers). Opportunity to break the impasse between utility and local investment and control in grid/power modernization and management of grid balancing with renewables.
- A base for on site production of H2 for Fuel Cell Vehicles.



Backup Slides



Reciprocating Engine Benchmarks

Table 1. Summary of distributed generation technologies

| | | | | | r Distribute | <u> </u> | | <u> </u> | | | |
|---------------------|--------------------|-----------------|-------|------------------------|--|--------------|-----------------------------|---|--|-------------------------------------|-----------|
| | Size Range (kW) | Efficiency(%) | | Emissions (g/kWh) | Foot print(sqft/kW) | | Installation Cost (\$AW) | Electric- Cost- to-Gen. (cents/kWh) | Cogeneration Cost -to- Gen.(c/kWh) | Maintenance Costs (cents/kWh) | |
| | | Electric | Ove | erall | щ <i>-</i> | prin | Pac | ч ў | Ele (C | రొత | Wi O |
| | | | | | R | eciprocating | Engines | | | | - |
| Spark Ignition | 30-5.000 | 31-42 | | | Nox:0.7-42 CO:0.8-27 | 0.28-37 | 300-700 | 150-600 | 7.6-13.0 | 6.1-10.7 | 0.7-2.0 |
| Diesel | 30-5.000 | 26-43 85-90 | | Nox: 6-22 CO: 0.1-8 | 0.22-0.31 | 200-700 | 150-600 | 7.1-14.2 | 5.6-10.8 | 0.5-1.5 | |
| Dual Fuel | 100-5.000 | 37-42 80-85 | | Nox: 2-12 CO: 2-7 | 0.15-0.25 | 250-550 | 150-450 | 7.4-10.7 | 6.0-9.1 | | |
| | · · · · | | • | | Tu | rbines | | | | | |
| | Non-Recup | | 14-20 | 75-85 | Nox: 9- | 0.15-0.35 | 700-1.000 | | 14.9-22.5 | 10.1-15.9 | 0.8-1.5 |
| Microturbines | Recup. | 30-200 | 20-30 | 60-75 | 125ppm CO: 9- 125ppm | 0.15-0.35 | 900-1.300 | 250-600 | 11.9-18.9 | 10.0-16.8 | |
| Industrial Turbines | | 1.000- 5.000 | 20-40 | 70-95 | Nox: 25- 200ppm CO: 7- 200ppm | 0.02-0.61 | 200-850 | 150-250 | 8.7-15.8 | 5.8-12.2 | 0.4-1.0 |
| | | | | | Fue | l Cells | | | | | |
| PEM | | 5-10 | 36-50 | 50-75 | Nox: 0.007 CO: 0.01 | 0.9 | 4.000- 5.000 | 400-1.000 | 21.9-33.3 | 20.7-33.3 | 0.19-1.53 |
| Phosphoric Acid | | 200 | 40 | 84 | Nox: 0.007 CO: 0.01 | 0.9 | 3.000- 4.000 | 360 | 18.6-22.8 | 17.0-21.2 | |
| | | | • | | Ren | ewable | | | | • | |
| P۱ | 7 | 5-5.000 | NA | NA | NA | NA | 5k-10k | 150-300 | 18.0-36.3 | N/A | 0.3-0.7 |
| Wind | | 5-1.000 | NA | NA | NA | NA | 1k-3.6k | 500-4k | 6.2-28.5 | N/A | 1.5-2.0 |

A Comprehensive Study on Microgrid Technology 2015.pdf

Neighborhood Energy Station Economics Model

| Nameplate power, MW 1.5 | efficiency, % | NH3 feed rate, full, ga/ hour 231 | Available heat, 40% mmbtus/hr 4.54 | | mWh per year at 100% 13,140 | MMBTU per year at 100% 39,805 | | NH3 feed tonnes per year, 100% 4672 | Pure h20 gal/yr at 100% 1,962,287 | | Ammonia cost, \$/tonne <mark>\$250</mark> | Annual NH3 spend at spec rate, MM\$ \$ 1.05 |
|---|--|---|--|---|--|---|--|---|---|--------------------------------------|--|--|
| Genset capex rate installed, \$/kw \$ 800 | CAPEX, MM\$ | Microgrid controller/ converter MM\$ \$ 0.15 | Land, Bldg, Tank, MM\$ \$ 0.20 | CAPEX MM\$ \$ 1.55 | Interest rate for debt 6.0% | % Equity invest 5 75% | Initial loan (15 yr), MM\$ \$ 0.388 | Debt payment MM\$ / yr \$0.040 | Sustaining Capital Rate 1.5% | | CAPEX charge MM\$ / yr \$ 0.063 | |
| % yr base operations 75.0% | operations | | Base Electricity \$/mWh \$ 100.0 | Premium Electricity, \$/Mwh \$ 200.0 | Total Electricity Revenue, MM\$/yr \$ 1.38 | Heat, \$/mmbtu 8.0 | Heat revenue, MM\$/yr 0.29 | Total Revenue, MM\$ \$ 1.67 | | Annual profit (MM\$/yr) \$0.40 | NPV10 MM\$/yr \$3.1 | IRR, overnight build 34.2% |
| | | | | | | | | | | | | |
| Nameplate power, MW | | NH3 feed rate, full, ga/ hour | Available heat, 40% mmbtus/hr | | mWh per year at 100% | MMBTU per year at 100% | | NH3 feed tonnes per year, 100% | Pure h20 gal/yr at 100% | | Ammonia cost, \$/tonne | Annual NH3 spend at spec rate, MM\$ |
| 1.5 | 45.0% | 231 | 4.54 | | 13,140 | 39,805 | | 4672 | 1,962,287 | | <mark>\$ 350</mark> | \$ 1.55 |
| Genset capex rate installed, \$/kw \$ 800 | Genset CAPEX, MM\$ | Microgrid controller/ converter MM\$ \$ 0.15 | Land, Bldg, Tank, MM\$ \$ 0.20 | CAPEX MM\$ \$ 1.55 | Interest rate for debt 6.0% | % Equity invest 75% | Initial Ioan (15 yr), MM\$ \$ 0.388 | Debt payment MM\$ / yr \$0.040 | Sustaining Capital Rate 1.5% | | CAPEX charge MM\$ / yr \$ 0.063 | |
| % yr base | % yr premium operations 20.0% | % yr offline 5.0% | Base Electricity \$/mWh \$ 120.0 | | Total Electricity Revenue, MM\$/yr \$ 1.71 | Heat, \$/mmbtu | Heat revenue, MM\$/yr 0.30 | Total Revenue, MM\$ | | Annual profit (MM\$/yr) | NPV10 MM\$/yr | IRR, overnight build |

Indicative Economics NH3 Plant

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http://www.wsj.com/articles/drillers-get-super-size-natural-gas-output-1441127955

Drillers Unleash 'Super-Size' Natural Gas Output

Applying newer fracking methods to existing field offers potential for more and cheaper fuel

So far, the impressive results have been confined to a small area in a single Louisiana parish near the Texas border. But if the approach works across the giant Haynesville Shale, which spans 120 miles across both states, the era of low American gas prices could extend for decades into the future, experts say.

"There's a large likelihood that the United States will be enjoying very low gas prices for a very long time, maybe 20 years," said Mark Papa, who has monitored Haynesville developments as a partner at Riverstone Holdings LLC, one of the biggest energy-focused private-equity firms in the U.S.

In August, Comstock officials told investors that it could get a 30% return on its new wells even with gas at \$2.50 a million BTUs. The Frisco, Texas-based company plans to drill more wells in Louisiana's Haynesville than it will in the oily Eagle Ford Shale in South Texas.

30% return with \$2.50 gas. Guaranteed offtake at \$300 per tonne approximately 10% IRR (without CO2 sales). No need for pipeline or market risk.



http://ac.els-cdn.com/S1876610214023601/1-s2.0-S1876610214023601-main.pdf?_tid=4d916e58-51e5-11e5-9954-00000aacb361&acdnat=1441248279_2c9af880201e68dff70b73f374ca07c0



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Energy Procedia 63 (2014) 5153 - 5163

Energy Proc

GHGT-12

Physicochemical factors impacting CO₂ sequestration in depleted shale formations: The case of the Utica shale

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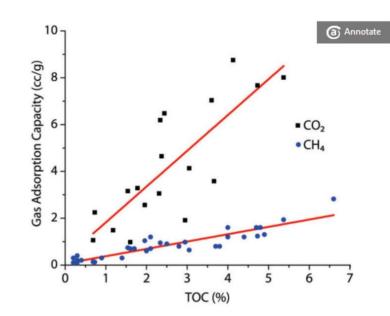
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Over the past several years, a number of groups have proposed the use of fractured shale formations that have been depleted of hydrocarbons as target repositories for GCS [5]–[8]. Depleted shale formations have a number of benefits over other repositories. Most importantly, the production of gas and oil from these formations means that a large amount of pore space has been opened and the resulting volume could be used to fill with CO_2 without creating significant over pressurization in the subsurface that could contribute to leakage. Further, the chemistry of the shale matrix is such that the kerogen in the shale preferentially sorbs CO_2 over CH_4 . That means a significant fraction of the injected CO_2 would adsorb to the kerogen surface rather than being mobile in the fracture network [9].

In addition to these and other physicochemical characteristics that make injection into depleted shales attractive, there are a number of logistical considerations that would make injection into fractured shales appealing. The well infrastructure used to produce gas can be repurposed for injection. This would dramatically cut down on the cost of injecting CO_2 into the subsurface [8]. At the surface, the gas pipeline distribution network could also be used to minimize the amount of new infrastructure that would be required to move the CO_2 to the wellhead. Finally, the understanding of the subsurface environment, and the monitoring that is already in place at many of these sites, would not need to be duplicated if the same wells were used for injection.

Our model was initially applied to the Marcellus shale and it was found that over the coming decade, the Marcellus shale alone could sequester over 1 Gigatonne of CO_2 each year. This is significant given that the US as a whole produces approximately 6 Gt of CO_2 each year, of which a little over 2 Gt are from stationary sources, like power plants, which can have their CO_2 readily captured and used in carbon storage. Cars and buildings, in contrast, are more dispersed and so their ability to capture CO_2 is much lower. The Marcellus shale was selected to demonstrate the model's capabilities because it is one of the first shale plays in the United States to receive large scale production and several years of data is available with production logs for a number of unconventional wells.

Enough room for free co2 output from 1,000,000 800 ktpa nh3 plants



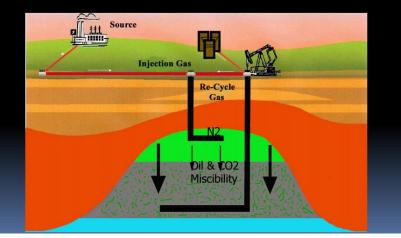


EXHAUST GAS INJECTION EOR

- Proven production increases up to 50X current production.
- Mobile generate gas at wellhead, no gas or CO2 pipeline cost.
- Green dual fuel source, propane or methane.
- Volume 1-Mmcfd modular units, trainable to any volume/flowrate
- Pressure as required, from low pressure to >2,000-psi injection.
- Drive N2 segregates; forms gas drive to push Oil/CO2 thru porespace
- CO2 lowers oil viscosity; swells oil up to 50% for greater mobility.
- Thermal gas up to 900*, alternative to Steam Flood, without water.
- Patented Process Weatherford Intl, exclusive licensing partner.

Gas Cap Injection + Gravity Drainage

Injected Gas Mixture (CO2+N2) Fills Reservoir Gas Cap N2 Pushes CO2 to Mix With Oil and Flow to Production Well



Exhaust Gas CO2 EOR

Exhaust Gas (CO2 + N2)

- Combustion gas from a standard internal combustion engine provides an ideal gas for enhanced oil recovery. Combustion gas is comprised of approximately 13% CO2 and 87% Nitrogen.
- Researchers at Louisiana State University compared the exhaust gas to pure 100% CO2 in simulated conditions and found that exhaust gas has significantly better performance than pure CO2 in the recovery of crude oil.
- In a pure CO2 flood, the CO2 combines with the oil under miscible pressure, doubling the volume of the oil and reducing the viscosity. This allows the oil to flow more freely towards the producing well. The CO2, however, does not provide drive. In a pure CO2 flood, gas injection is followed by water (WAG, Water And Gas), which provides pressure and drive to push the oil towards a producing well.
- In an exhaust gas flood the 13% CO2 separates from the Nitrogen, and combines with the oil under pressure, providing the needed swelling and increase in oil flow. Meanwhile, the 87% Nitrogen gas rises to the top of the reservoir, providing a pressure source which is more effective than water at driving oil towards a producing well.

Exhaust Gas Applications

Enhanced Oil Recovery

- Pinnacle reefs, primary recovery 25%
- Most conventional reservoirs are candidates
- Unconventional Shales new studies show 10% added EUR
- Incremental oil recovery after water-flood
- CHOPs re-pressurization & heating
- Alternate EOR versus water-flood

Enhanced Gas Recovery - EGR

- Re-pressure depleted natural gas reservoirs
- Sweep gas for natural gas reservoirs (CBM)
- Gas over oil replacement (Surmont)

Thermal applications

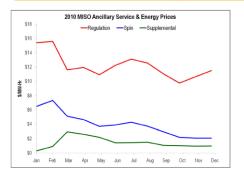
- Gas temperature up to 900*
- low Gravity Heavy Oil reservoirs
- Alternative to SAGD

Reciprocating Engine Characteristics

Time Scales for Ancillary Services







The following characteristics outline the benefits of medium speed engine technology for ancillary services:

Operating Flexibility

- 3 minute starting time
- Zero startup cost
 - MW/minute ramp rate
- Regulation (AGC) accuracy
- Minimum load
 - % load on each engine
 - Multi engine plant
- Cost
 - Relatively low capital cost
 - Excellent efficiency
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 - Reduction through SCR/OxyCad's
- Installation speed
- Siting flexibility
 - Transmission constraints
 - Transmission alternative*
- Reactive power
 - Synchronous condenser clutch?
- Black start
- Islanded operation

CAT

Products for Ancillary Services



CAT





Cost Analysis: Utilizing Used Li-Ion Batteries.

- A new 15 kWh battery pack currently costs \$990/kWh to \$1,220/kWh (projected cost: 360/kWh to \$440/kWh by 2020).
- The expectation is that the Li-Ion (EV) batteries will be replaced with a fresh battery pack once their efficiency (energy or peak power) decreases to 80%. Based on various forecasts for market penetration of PHEVs and EVs over the next 10 years, a large number of PHEVs and EVs will be approaching this 80% efficiency level by 2020. These batteries can be recycled or used in other less demanding applications for the rest of their useful life provided a business case can be made for their secondary use.
- The minimum goal for a selling price for a Used Li-Ion Batteries is less than \$150/kWh for 25,000 units at 40 kWh.

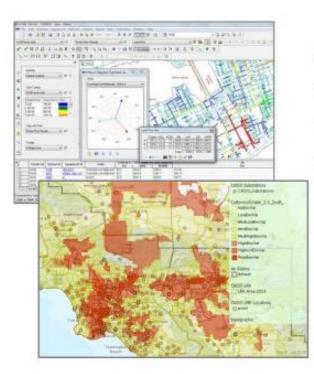
Economic Analysis of Deploying Used Batteries in Power Systems by Oak Ridge NL 2011

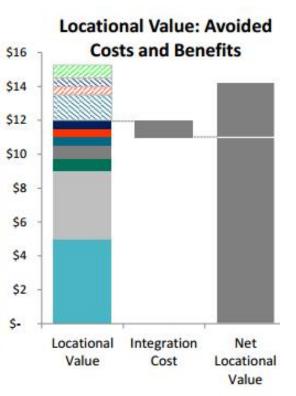


Ammonia Energy Station can be installed at highest locational value Highest leverage to stabilize grid, relieve congestion and defer infrastructure investment

For Each DPA & Substations/Feeders Annual Dist. Planning & Integration Capacity Analyses Biennial DRP Locational Value Analysis







http://resnick.caltech.edu/docs/MTS_V2.pdf

Utility Level Storage to Stabilize Grid

Utility Storage Market Drivers:

- Wind and Solar Integration
- Energy Arbitrage
- Frequency Regulation & Ancillary Services
- Infrastructure Upgrade Deferral
- Locational Capacity

Different battery technologies will supply this market



120kW – 500kW Bonneville Power Authority, WA

Ideal Power is forming alliances with leading battery suppliers







AQUION

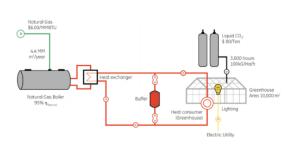
IDEAL 💽 POWER

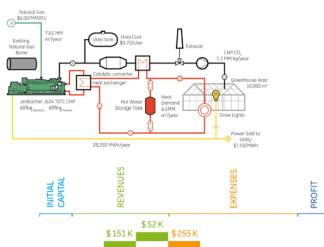
http://www.evernote.com/l/ALbpbSDydxdBU50aQaAN7yugZqO3SDOKX54/

The economic benefits of the CHP solution for greenhouses can be seen at a 25-acre (10-hectare) tomato greenhouse in the U.S. when compared to an installation with natural gas-fired boilers. The greenhouse illustrated here has installed a Jenbacher J624 gas engine with two-stage turbocharging and an output of 4.35 MW. It runs 6,600 hours per year and has heat coverage of 73.5 percent.

After

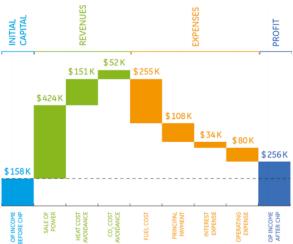
Before





The breakdown

- Operating income increased by 62 percent through sales of excess power
- Installed system cost was \$7 million, 80 percent of which was debt-financed at a 6 percent interest rate for 10 years
- Pre-tax payback is projected at 4.7 years



Profits shown are based on a 25-acre (10-hectare) tomato greenhouse in the U.S.



| NEIG | нво | RHOOD ENE | RGY STATI | ON (LIKE A O | GAS STATIO | N) Dispensi | ng 1.75 MM | Gals Per Ye | ar Of Amm | onia | | | | | |
|--|--------------------------|--|---|--|--|--|--|---|---|--|---|--|--|--|--|
| MOD | EL RESL | ILTS | | | | COST, T | HERMO AND CO2 | MATRIX | | | | | | | |
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME | | | |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 4,060 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | INPUT Price of methanol delivered to site, \$ | INPUT Price of DME delivered to site, \$ / tonne | | | |
| OPTIONAL USER | | 1 | | a constant? | | | | | | | / tonne | | | | |
| DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NH3 BASIS) IN CS. ITERATE D4 TO ACHEVE DESIRED QUANTITY IN DS | | 0.00 | | \$350 | \$15.00 | \$3.00 | \$2.00 | \$3.80 | \$50 | \$3.00 | \$200 | \$290 | | | |
| MMBTU (or 1000 CF gas | 21.32 | 86,558 | | MMETU gas for 21.3 Gal gaseline for 21.3 Gal U/G for 21.3 MMETU MARTU MA | | | | | | | | | | | |
| MMBTU gas required for | 32.0 | 129,930 | | 14 | 21.1 | 172 | 234 | 15 | | 253 | 0.942 | Tonnes DME for 21.3 MMBTU 0.71 | | | |
| TCF natural gas required | 2.945-08 | 0.000 | | NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 | Gasoline Fuel Cost (for 21.3 mmbtu) - This | LPG Fuel Cost (for 21.3 mmbtu) - This Scenario | Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario | Coal Fuel Cost (for 21.3 mmbtu) - This Scenario | Ethanol Fuel Cost (for 21.3 mmbtu) - This | Methanol Fuel Cost (for 21.3 mmbtu) - | OME Fuel Cost (for 21.3 mmbtu) - This | | | |
| Tonnes water produced | 1.588+00 | 6,415 | | \$350 | \$320 | Scenario \$516 | \$468 | \$593 | \$53 | Scenario \$759 | This Scenario \$196 | Scenario \$206 | | | |
| # Global ammonia | 6.678-09 | 0.000 | | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at | kwh from 21.3 mmbtu a | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% | kwh from 21.3 mmbtu at 45% | | | |
| industry If of World Scale NH3 | 1.258-66 | 0.01 | | like) | like) | 35% efficiency (coal like) | (ke) | 35% efficiency (coal like) | 35% efficiency (coal like) | like) | efficiency (gas/nh3 | efficiency (gas/nh3 2800 | | | |
| Plants Number of 60,000 cbm | 2.448-05 | 0.01 | | Fuel cost for power, | Fuel cost for power for | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | | | | |
| vessels Number of 80 tonne | | 0 | | Fuel cost for power, \$/kwh from NH3 | Fuel cost for power for power, S/kwh from gas | Fuel cost for power, S/kwh from gasoline | Fuel cost for power, \$/kwh from LPG | Fuel cost for power, \$/kwh from diesel | Fuel cost for power, 5/kwh from coal | Fuel cost for power, S/kwh from coal | 5/kwh from methanol | Fuel cest for power, \$/kwh from DME | | | |
| railcar deliveries | 0.0125 | 51 | AMMONIA, NO | \$0.125 AMMONIA w/ | \$0.114 | \$0.235 | \$0.167 | \$0.269 | \$0.024 | \$0.271 | \$0.070 | \$0.074 | | | |
| MWh from 45% efficient | 1.005-06 | 0.0 | CCS T CO2 per 21.3 | HARVEST T CO2 per 21.3 | NATURAL GAS | GASOLINE T CO2 per 21.3 mmbtu, | LPG T CO2 per 21.3 mmbtu, | DIESEL T CO2 per 21.3 mmbtu, | COAL T CO2 per 21.3 mmbtu, | ETHANOL T CO2 per 21.3 mmbtu, | METHANOL T CO2 per 21.3 | DME T CO2 per 21.3 | | | |
| NWh from 45% efficient power plants | 2.818+00 | 11,410 | mmbtu,only production, no CCS | CO2 harvest | NOT COUNTING UFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING UFECYCLE | COUNTING LIFECYCLE | COUNTING LIFECYCLE | | | |
| can be run for 1 year, 45% | 3.218-05 | 0.1 | 1.93 | 0.68 | 1.23 | 1.65 | 1.48 | 1.68 | 2.42 | 0.33 | 1.80 | 1.80 | | | |
| Equivalent # of 6 mtpa LNG train (8TU basis) | 6.875-08 | 0.00 | | | | | NOTES | | | | | | | | |
| Tonnes LNG equivalent | 0.41 | 1,665 | 5252 | Local Energy Station Dispensing 1.75 Mm Gals Per Year Of Ammonia | | | | | | | | | | | |
| Metric Tonnes coal equiv | 1.04 | 4,223 | examines a 'ne | A typical high volume gasoline station can easily dispense 1.5 MM gallons of multiple grades of gasoline/diesel in a year. This case examines a 'neighborhood' ammonia energy station of approximately the same scale that could provide power and heat to the | | | | | | | | | | | |
| Tonnes oil equivalent (TOE) | 0.500 | 2,030 | neighborhood (or condo or office building) in an urban environment. This station would house a diesel genset/CHP unit running on ammonia. The prototype for this is the MHI MegaNinja gas-driven genset (delivered on 40° trailer, 1.5 MW generator operating at 42.5% | | | | | | | | | | | | |
| Tonnes resid equiv | 0.530 | 2,152 | efficiency, designed for combined heat/power taking efficiency up to 75% for medium pressure steam/space and water heating and adsorptive air conditioning.) | | | | | | | | | | | | |
| Gal LPG equiv | 234 | 950,116 | The general co | The general complexity of these stations would be less than a gasoline station (single grade, dispensed almost entirely to the generators | | | | | | | | | | | |
| Gal Gasoline equiv | 172 | 698,376 | instead of retail interface with hundreds of transactions to untrained public per day). But tank volume, general regulatory requirements and fuel delivery logistics would be similar. | | | | | | | | | | | | |
| Gal Ethanol equiv | 253 | 1,027,262 | The average we | and the Genery reports would be animat. The average weekly volume would be about 35,000 gallons. We can 'design' for 40,000 gal/week peak usage. A typical tank size for | | | | | | | | | | | |
| Gal Ethanol equiv | 253 | 1,027,262 | The average we | The average weekly volume would be about 35,000 gallons. We can 'design' for 40,000 gal/week peak usage. A typical tank size for | | | | | | | | | | | |
| Price NH3 | \$350 | | temp/pressure | maintenance), w | e could operate w | ne 30,000 gal tan ith three a week o | leliveries from 11 | 500 gal tank truck | security and ease | of monia trucks). | | | | | |
| Total NH3 cost \$ | | 1,421,114 | | | | I that, but this will | | | | | | | | | |
| Fuel cost for power, \$/kwb from MH3 | \$ 0.125 | | Very rough pro Roughly \$1.5-\$ | | be about \$1.2 MM | A for ammonia M | egaNinja, \$0.1 Mi | M for undergrour | id tank, connectio | ons and land. | | | | | |
| Price NATURAL GAS | \$15.00 | | With these deli | ivery assumptions | (1.75 MM gal am | monia/year), a 1. | MW Meganinja | can be supplied 8 | 5% of the time (.1 | 3/.15). The unit | | | | | |
| Total Natural Gas cost \$ | | \$ 1,297,274 | would be availa model this as | able 100% of the t | ime (minus maint | enance) and could | be run at the cos | t of more freque | nt ammonia delive | eries. We can | | | | | |
| Fuel cost for power for power, S/kwh from gas | \$ 0.114 | | A CHP unit that | t is integrated into | the local electric | al grid, sells exces | power into the g | rid and buys pow | er from the grid w | hen power is | | | | | |
| power, S/kwh from gas Price GASOLINE | \$3.00 | | offered at belo | w cost/value of lo | cal power and he | at supply. For example ak power dema | mple, buying low | cost base load pov | wer at night from | utility based on | | | | | |
| Total Gasoline cost \$ | | \$ 2,095,128 | 97. 1986. | | | for 7450 hrs for 1 | | | of CHP heat (calcu | ulated as 30% of | | | | | |
| Fuel cost for power, | \$ 0.235 | | the mmbtu's in or sold. | the 1.75 mm gal | of ammonia)). W | e will assume con | servatively that 15 | 5,000 mmbtu of th | hat heat would be | effectively used | | | | | |
| S/kwh from gasoline Price LPG | \$2.00 | | | . 1.75 mm tonnes | of ammonia costs | \$1.2 MM | | | | | | | | | |
| Total LPG cost \$ | | \$ 1,900,232 | | | | environments, the | n \$0.14 per kwh | and \$14 per MMR | TU are conservati | ve prices for | | | | | |
| Fuel cost for power. | \$ 0.167 | s,swi,232 | residential cust | omers (especially | conservative in t | he winter). Sales (57 MM for powe | or avoided costs of | of gas/power pure | hases) of the pow | | | | | | |
| \$/kwh from LPG | | | | | | even rejecting all | | | | al 15% of the | | | | | |
| Price DIESEL | \$3.80 | | year that kwh a | are valued at high | er than \$0.11 per | even rejecting all kwh, the generato rices are uniform | r can be operated | for additional pr | ofit. For example | , in New | | | | | |
| Total Diesel cost \$ | | 5 2,406,961 | | | | at a margin of \$0. | | | | Att 0111 101 13% | | | | | |
| Fuel cost for power, S/kwh from diesel | \$ 0.269 | | | ery rough number | s running the busi | iness blind (i.e, sel | ling at average pr | ices, managing CH | IP heat and extra | power sales | | | | | |
| Price COAL | \$50 | | | 00/tonne - \$1,200 | | | | | | | | | | | |
| Total Coal cost \$ | | \$ 211,137 | Opportunistic s | ales of power for | other 15% of gen | t conservative pri erating capacity - | ces) - \$1,780,000 \$100,000 | | | | | | | | |
| Fuel cost for power, \$/kwh from coal | \$ 0.024 | | | | o cover capex/op | ex/profit. | | | | | | | | | |
| Price ETHANOL | \$3.00 | | | al on these reven | | | | | | | | | | | |
| Total Ethanol cost \$ | | \$ 3,081,787 | | | M (market to pay ot). This is \$73,00 | for guaranteed ca 0 per year. | pacity in PJM grid |). In New York, th | is is about \$200 p | er MW (paid | | | | | |
| Fuel cost for power, \$/kwh from ethanol | \$ 0.271 | | Potential paym | ents from reliabil | ity premiums from | n the grid (this pow | | | provided power (| no risk from gas | | | | | |
| MegaTonnes CO2 saved with NH3 with harvest vs GAS | 5.508-07 | 0 | deliverability, d | lowned power lin | es, frozen equipm | ent, price spikes f | rom hot summer | afternoons, etc). | | | | | | | |
| | | | _ | | | | | | | | | | | | |

Local Energy Station Dispensing 1.75 Mm Gals Per Year Of Ammonia

A typical high volume gasoline station can easily dispense 1.5 MM gallons of multiple grades of gasoline/diesel in a year. This case examines a 'neighborhood' ammonia energy station of approximately the same scale that could provide power and heat to the neighborhood (or condo or office building) in an urban environment. This station would house a diesel genset/CHP unit running on ammonia. The prototype for this a gas-driven genset (delivered on 40' trailer, 1.5 MW generator operating at 42.5% efficiency, designed for combined heat/power taking efficiency up to 75% for medium pressure steam/space and water heating and adsorptive air conditioning.)

The general complexity of these stations would be less than a gasoline station (single grade, dispensed almost entirely to the generators instead of retail interface with hundreds of transactions to untrained public per day). But tank volume, general regulatory requirements and fuel delivery logistics would be similar.

The average weekly volume would be about 35,000 gallons. We can 'design' for 40,000 gal/week peak usage. A typical tank size for ammonia distributors is 30,000 gallons. So, with one 30,000 gal tank (installed underground for safety, security and ease of temp/pressure maintenance), we could operate with three a week deliveries from 11,500 gal tank trucks (typical size ammonia trucks). I'm sure the logistics can/will be optimized beyond that, but this will do for illustration.



ΖU

Energy Storage for the Electricity Grid: Benefits and Market Potential Assessment Guide

A Study for the DOE Energy Storage Systems Program

Table ES-1. Summary of Key Assumptions and Results

| | | | narge tion* | | acity kW, MW) | Benefit (\$/kW)** | | Potential (MW, 10 Years) | | Economy (\$Million) [†] | |
|------|---|---------|----------------|-----------------|-------------------------|----------------------|-------------|-----------------------------|--------|-------------------------------------|--------|
| # | Benefit Type | Low | High | Low | High | Low | High | CA | U.S. | CA | U.S. |
| 1 | Electric Energy Time-shift | 2 | 8 | 1 MW | 500 MW | 400 | 700 | 1,445 | 18,417 | 795 | 10,129 |
| 2 | Electric Supply Capacity | 4 | 6 | 1 _{MW} | 500 MW | 359 | 710 | 1,445 | 18,417 | 772 | 9,838 |
| 3 | Load Following | 2 | 4 | 1 MW | 500 MW | 600 | 1,000 | 2,889 | 36,834 | 2,312 | 29,467 |
| 4 | Area Regulation | 15 min. | 30 min. | 1 MW | 40 MW | 785 | 2,010 | 80 | 1,012 | 112 | 1,415 |
| 5 | Electric Supply Reserve Capacity | 1 | 2 | 1 _{MW} | 500 MW | 57 | 57 225 | | 5,986 | 90 | 844 |
| 6 | Voltage Support | 15 min. | 1 | 1 MW | 10 MW | 4(| 400 | | 9,209 | 433 | 5,525 |
| 7 | Transmission Support | 2 sec. | 5 sec. | 10 MW | 100 MW | 192 | | 1,084 | 13,813 | 208 | 2,646 |
| 8 | Transmission Congestion Relief | 3 | 6 | 1 MW | 100 MW | 31 | 141 | 2,889 | 36,834 | 248 | 3,168 |
| 9.1 | T&D Upgrade Deferral 50th percentile ⁺⁺ | 3 | 6 | 250 kW | 5 MW | 481 | 687 | 386 | 4,986 | 226 | 2,912 |
| 9.2 | T&D Upgrade Deferral 90th percentile ⁺⁺ | 3 | 6 | 250 kW | 2 MW | 759 | 1,079 | 77 | 997 | 71 | 916 |
| 10 | Substation On-site Power | 8 | 16 | 1.5 kW | 5 kW | 1,800 | 1,800 3,000 | | 250 | 47 | 600 |
| 11 | Time-of-use Energy Cost Management | 4 | 6 | 1 kW | 1 MW | 1,2 | 1,226 | | 64,228 | 6,177 | 78,743 |
| 12 | Demand Charge Management | 5 | 11 | 50 kW | 10 MW | 51 | 82 | 2,519 | 32,111 | 1,466 | 18,695 |
| 13 | Electric Service Reliability | 5 min. | 1 | 0.2 kW | 10 MW | 359 | 978 | 722 | 9,209 | 483 | 6,154 |
| 14 | Electric Service Power Quality | 10 sec. | 1 min. | 0.2 kW | 10 MW | 359 | 359 978 | | 9,209 | 483 | 6,154 |
| 15 | Renewables Energy Time-shift | 3 | 5 | 1 kW | 500 MW | 233 | 389 | 2,889 | 36,834 | 899 | 11,455 |
| 16 | Renewables Capacity Firming | 2 | 4 | 1 kW | 500 MW | 709 | 915 | 2,889 | 36,834 | 2,346 | 29,909 |
| 17.1 | Wind Generation Grid Integration, Short Duration | 10 sec. | 15 min. | 0.2 kW | 500 MW | 500 | 1,000 | 181 | 2,302 | 135 | 1,727 |
| 17.2 | Wind Generation Grid Integration, Long Duration | 1 | 6 | 0.2 kW | 500 MW | 100 | 782 | 1,445 | 18,417 | 637 | 8,122 |

*Hours unless indicated otherwise. min. = minutes. sec. = seconds.

**Lifecycle, 10 years, 2.5% escalation, 10.0% discount rate.

[†]Based on potential (MW, 10 years) times average of low and high benefit (\$/kW).

¹¹ Benefit for one year. However, storage could be used at more than one location at different times for similar benefits.



Downtown Chicago keeps cool with ammonia chillers

02 February 2012



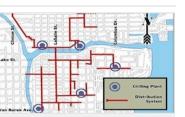
Beneath the streets of downtown Chicago a network of pipes distributing chilled water forms part of one of the world's largest interconnected district cooling systems. Ammonia chillers, ice tanks and river water chillers provide cooling for building air conditioning, removing on peak grid stress. The system will take centre stage in June 2012 when IDEA holds their annual conference in Chicago.

Thermal Chicago's district cooling system serves around a hundred buildings and upwards of 45 million square feet (4 million m2) of space. The company's customers include commercial and industrial facilities, office towers, condominiums, apartment buildings, theatres, hotels, data centres, retail centres and schools.

Chicago's district cooling system

In 1995, the first source of chilled water came online, called plant one, or P1, located at junction of State and Adams. At the time the nascent district cooling system only had 11 customers. The following year the largest plant, P2, came online. It contains the world's largest ice tank that can deliver 125,000 tonne-hours of cooling to the system and holds two million gallons (7 millions litres) of chilled water.

In the basement of the Blue Cross/Blue Shield of Illinois headquarters on Randolph Street you can find P3, housing three large ice tanks and an ammonia chilling plant. The ammonia chillers and ice tanks replaced a previous 30,000 ton R22 plant, with P3 able to stay online during entire renovation, which started in 2008 and finished in 2010.



Chicago's district cooling network is one of the largest in the world

Related articles

How ammonia district cooling can be joined with desalination 12 December 2011



About natural refrigerants

As a general differentiation, "natural refrigerants" are substances that exist naturally in the environment, while "non-natural refrigerants" or "synthetic refrigerants" are man-made chemicals. The most commonly used natural refrigerants today are ammonia (NH₃, R717) carbon dioxide (CO₂, R744), and hydrocarbons (HCs), such as propane (R290), isobutane (R600a) and propylene, also know as propene (R1270).

The precision of the term "natural refrigerants" is sometimes debated, given that, to be used as refrigerants, ammonia, carbon dioxide, and hydrocarbons also undergo an industrial purification and manufacturing process. However, today there is a well established distinction between substances whose chemical properties and safety aspects have been studied in their entirety and fluorinated gases, which, given their chemical complexity and comparatively short period of usage, have confirmed and/or unknown negative effects on ozone depletion, global warming and ecological safety, and therefore, are subject to continued debate.

The most commonly used natural refrigerants today are ammonia (NH₂, R717), carbon dioxide (CO₂, R744) and hydrocarbons (HCs), such as propane (R290), isobutane (R600a) and propylene, also know as propene (R1270).

Mixtures of ammonia and dimethyl ether (R723) have been developed, as well as various hydrocarbon blends with optimized performance and safety properties (isobutane/propane, R441 etc.). Water as a refrigerant has been used especially in absorption and adsorption chillers. The use of air is less common, but has been developed for deep-freezing applications.



Ammonia (ODP= 0; GWP= 0)

Ammonia (chemical symbol NH₃, refrigerant designation R717) is a colorless gas at atmospheric pressure. With zero ozone depletion and global warming potential, as well as a short atmospheric lifetime, it does not form any by-products or decomposition products with negative environmental impact. It is compatible with some, but not all, commonly used refrigeration system lubricants. In particular, it is not suited for use with polyol ester (POE) and poly vinyl ether (PVE) lubricants, and it only has limited applications with poly alkylene glycol (PAG) lubricants.

Despite its undisputed energy efficiency benefits, the use of ammonia is restricted in certain applications and geographic regions, due to its toxicity. As a result, R717 is effectively prohibited from use inside occupied spaces but can be used in unoccupied areas or outside.

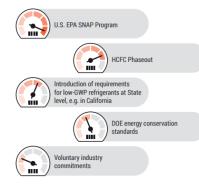
However, many advances have been made in recent years to minimize risks for human health, particularly for ammonia installations in populated areas. These advances include using ammonia in conjunction with other refrigerants, such as in secondary systems, in order to reduce and isolate an ammonia charge, using advanced safety equipment, deploying containment casings, or using ammonia absorption systems.

http://www.evernote.com/l/ALa9jFViPJVCo7m5QA2-oD9pWZWjyBxw9KU/

But even in the midst of limitations, since the last GUIDE, the list of positives has only expanded and the list of negatives attributed to natural refrigerants has diminished. An increased focus on safety has been mitigating concerns over flammability and toxicity, especially in the use of ammonia, which has been subject to increased scrutiny and fines from the EPA in order to reduce incidents and improve confidence.

The increased uptake in natural refrigerant-based systems is also lowering prices across all applications and there is hope of simplified solutions for both industrial and commercial applications, with packaged solutions becoming increasingly prevalent. Energy efficiency is also being increasingly linked with natural refrigerants, and solutions for warm-ambient climates, especially in commercial refrigeration, are being developed and tested extensively.

All of these positive impacts have meant that natural refrigerants in the three key applications –light commercial, commercial and industrial refrigeration – have all seen growth in the triple digits since 2013, with much untapped potential to be explored during the next five years if the market is able to assimilate itself quick enough to absorb and process the extra demand.



Several policy measures working together to accelerate uptake of natural refrigerants

At ATMOsphere America 2015, participants assessed through live polling a variety of policy measures in the U.S. in terms of their impact on accelerating the introduction of natural refrigerants through live polling. The EPA SNAP Program and the HCPC phase out are deemed to have the highest impact on accelerating the uptake of natural refrigerants, while voluntary industry initiatives are not believed to have a strong impact throughout the industry. But the advancements by Refrigerants, Naturally! and other companies can not be ignored.



Low Carbon Ammonia (And Front End For CCS)

- Ammonia plants emit pure (sequestration-ready) CO₂. Approximately 2/3 is pure. With current technology, the rest is flue gas from the reformer.
- There are active markets to purchase CO₂ for enhanced oil recovery.
- Ammonia plants built close to EOR fields can sell their waste CO₂ to be sequestered in oil fields after use. EOR technologies exist for complete CO2 sequestration at low incremental cost. (co-injection with N2)
- This co-product value can reduce production cost for eventual fuel use.
- These operations will also supply a great deal of experience and technology for carbon capture and for CO₂ transportation and sequestration.
- This will serve as a bridge while "green ammonia" technologies from renewables, hydro and nuclear energy are optimized for a decarbonized ammonia energy system for power and for liquid fuel for transportation.

