

# **Vanadium As a Potential Catalytic Membrane Reactor Material for NH<sub>3</sub> Production**

Simona Liguori and Jennifer Wilcox

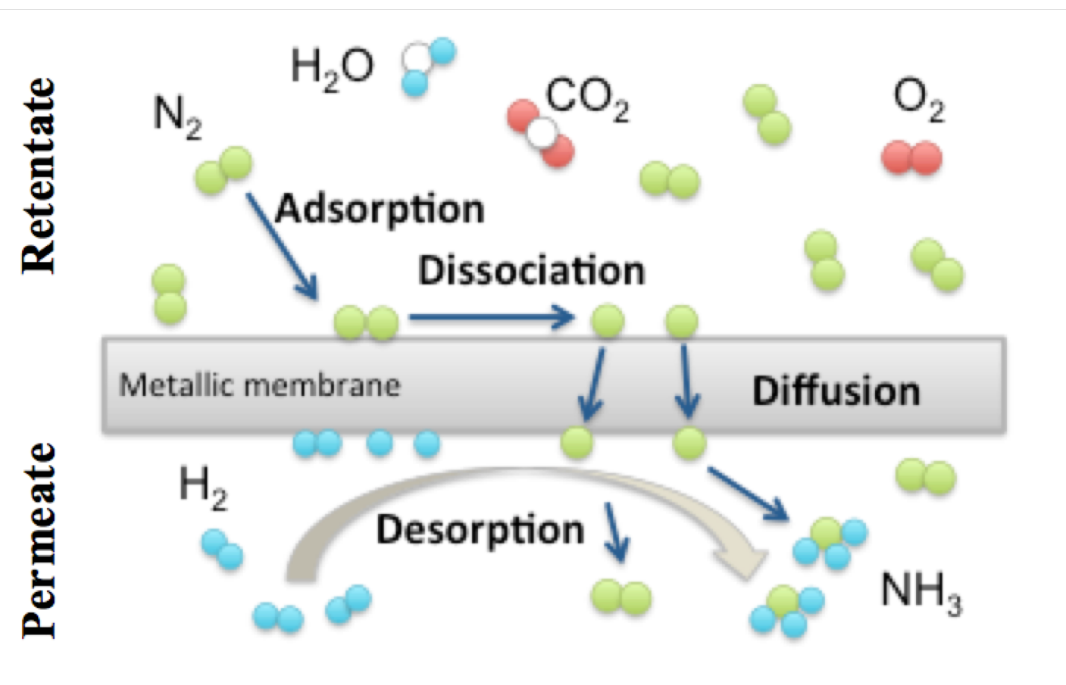
Worcester Polytechnic Institute

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# Aim

Ammonia production through a catalytic membrane reactor configuration using Earth-abundant metals for the  $N_2$ -selective membrane reactor at low pressure, up to 30 bar and low temperature 400 C, instead of the typical conditions used in the Haber-Bosch process.






# N<sub>2</sub> Selectivity Metallic Membranes – Low pressure

400 °C

*N<sub>2</sub> Permeating Flux [L/m<sup>2</sup>/day]*

$\Delta p$ [bar]	Nb	Ta	V
2	34	28	40
3	45	40	57
4	62	45	62
5	68	57	73

-  Metallic membranes (V, Nb, Ta) are entirely selective for N<sub>2</sub> over He and CO<sub>2</sub> ( $\alpha = \infty$ )
-  Fluxes are low
-  Metallic thin films, an order of magnitude thinner than foils, may lead to significantly higher fluxes

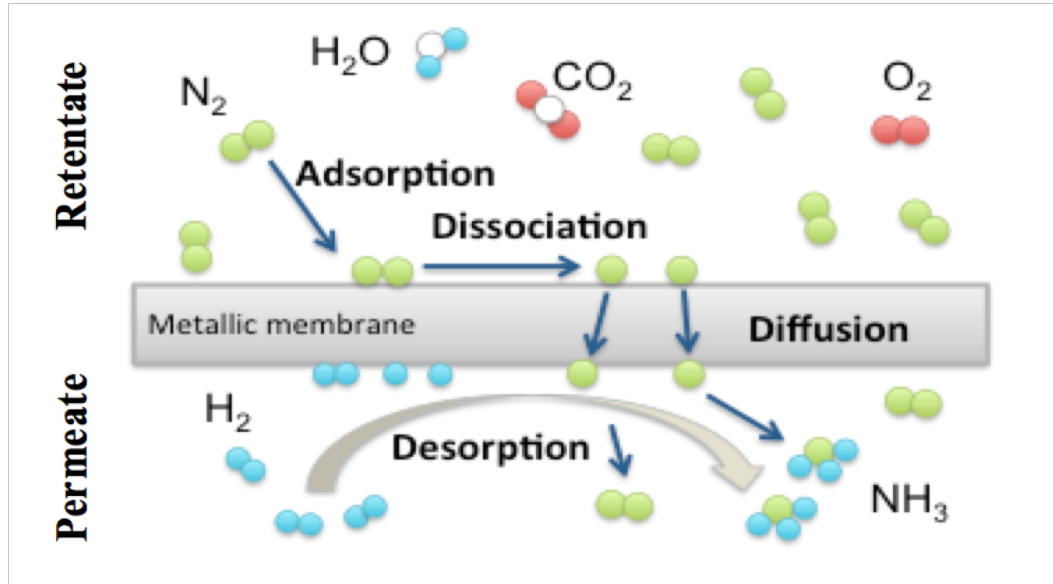
# N<sub>2</sub> Selectivity Metallic Membranes – High pressure

- At **each temperature**, no He and CH<sub>4</sub> were detected during the testing. Only N<sub>2</sub> permeated through the membrane.
- The following table shows the **comparison between V and Fe membranes** by performing permeation testing with pure N<sub>2</sub> at different temperature and pressure.

p [bar]	N <sub>2</sub> [L/m <sup>2</sup> /day]					
	<i>T = 400 – V</i>	<i>T = 400 – Fe</i>	<i>T = 500 – V</i>	<i>T = 500 – Fe</i>	<i>T = 600 – V</i>	<i>T = 600 – Fe</i>
30	116	88	239	158	402	15
40	156	125	352	225	603	26
50	216	165	465	311	828	33
60	271	211	577	376	1079	45

- V membrane shows better performance in terms of N<sub>2</sub> permeation with respect to Fe membrane.
- *At 600 °C, the N<sub>2</sub> permeating flux dropped dramatically.*

# Ammonia Synthesis by using V membrane



Data at 500 C and 60 bar – V membrane

	<b>NH<sub>3</sub> [mol/cm<sup>2</sup> s]</b>
Permeate side (1 bar)	3.91E-10
Retentate side (60 bar)	3.71E-10

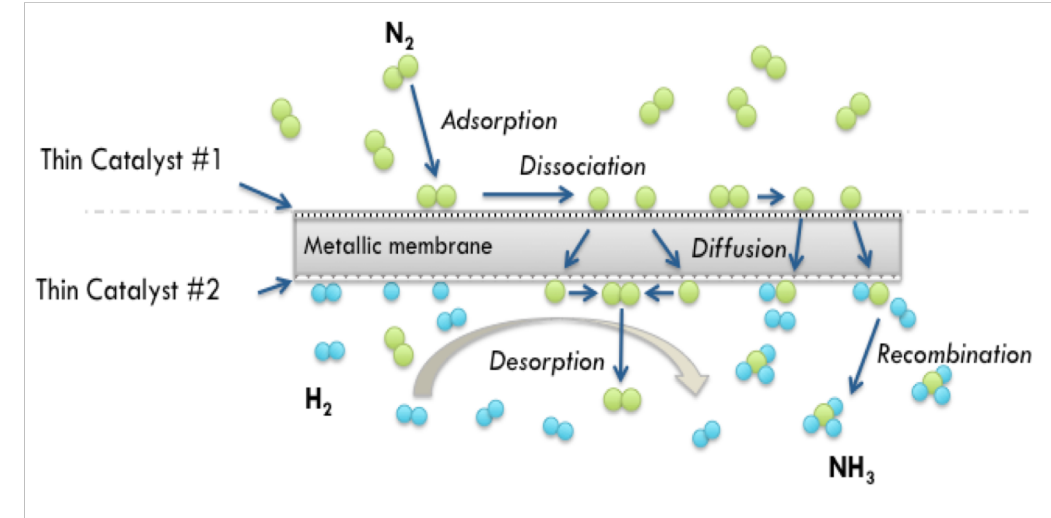
Only 5% of the permeate nitrogen reacts to form NH<sub>3</sub>

# Deposition of thin layer V-Ru on V membrane

A V-Ru thin layer (~150 nm) was sputtered on three V membranes.

V-Ru was sputtered on three different samples:

- Retentate side of the V membrane
- Permeate side of another V membrane
- Both sides of the V membranes



## V-Ru thin layer on V membrane – retentate side

- The membrane was characterized by permeation tests with pure gases.
- With respect the pure V membrane v-Ru/V showed an improved permeated flux.
- The improvement was approximately of 5% at each condition.

# Ammonia Synthesis by using V-Ru/V membrane

Data at 500 C and 60 bar – V-Ru/V membrane

	NH <sub>3</sub> [mol/cm <sup>2</sup> s]	NH <sub>3</sub> [mol/cm <sup>2</sup> s] (V membrane)
Permeate side (1 bar)	4.11E-10	3.91E-10
Retentate side (60 bar)	4.55E-10	3.71E-10

**Work in progress** on:

- V/V-Ru → where the thin layer of V-Ru is deposited on the permeate side
- V-Ru/V/V-Ru → where the thin layer is deposited on both sides of the membranes

# Conclusion

- V, Nb, Ta, Fe show infinite ideal selectivity with respect to He, CO<sub>2</sub> and CH<sub>4</sub> → only N<sub>2</sub> can permeate through the membranes
- N<sub>2</sub> permeation flux through the membrane is extremely low
- NH<sub>3</sub> production strongly depends on the N<sub>2</sub> permeation and the presence of catalyst

## Future Work

- Reduce the thickness of the metallic membrane
  - Prepare defect-free inorganic membrane able to work for long periods
  - Quantify ammonia production as a function of temperature, pressure gradient and membrane material
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**THANKS FOR  
YOUR KIND ATTENTION**